



Research Article

Numerical modelling of 3D magnetohydrodynamics chemically reacting permeable sheet influenced by free stream convection nanofluid flow

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ARTICLE INFO

Article history

Received: 29 February 2024

Revised: 11 October 2024

Accepted: 13 October 2024

Keywords:

Chemical Reaction;
Magnetohydrodynamics;
Nanofluid; Non-Newtonian
Casson Fluid; Permeable Sheet

ABSTRACT

The effects of a chemical reaction on mixed convective nanofluid flow along a permeable stretched surface in the presence of free stream flow are demonstrated. The impact of multiple non-dimensional characteristics on different gradients and profiles is investigated. Through appropriate transformations, governing coupled partial differential equations become ordinary differential equations, which are then solved numerically. Through MATLAB programming, Runge Kutta Fehlberg method by following shooting technique yields the numerical solutions. Influence of fluid parameters especially free stream velocity, thermal Biot number, concentration Biot number, heat generation parameter, chemical reaction parameter, stretching ratio parameter, permeability parameter, magnetic parameter, Prandtl number, Brownian motion parameter, Lewis number has been investigated that makes this research novel one. The calculated results are presented in the form of tables and contour plots. Furthermore, examined are the thermal transfer strength (Nusselt number) and the mass exchange strength (Sherwood number). According to our research, the velocity distribution gets smaller as the magnetic parameter increases, but the corresponding profile gets increases for free stream velocity flow. With rise in the values of stretching ratio parameter from 2.0-10.0, heat transfer rate falls down by 7.24%. Heat transfer rate falls down by 22.37% with rise in the values of Prandtl number within the range 0.2-1.0. Additionally, temperature enhances with enhancement in thermal Biot number. Comparing its latest findings to prior outcomes and accomplishing convergence criteria supports this technique's validity. Current research in this domain has diverse applications, encompassing power plants, refrigeration systems, medical science, ranging from transportation to energy production and in wide variety of industries, Micro-Electro-Mechanical Systems and in the field of biotechnology. This research attempts to help industrial companies achieve product quality by regulating transport phenomena.

Cite this article as: Yadav S, Kumar S, Sharma PK, Makkar V, Dang K. Numerical modelling of 3D magnetohydrodynamics chemically reacting permeable sheet influenced by free stream convection nanofluid flow. J Ther Eng 2025;11(3):845–857.

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This paper was recommended for publication in revised form by
Editor-in-Chief Ahmet Selim Dalkılıç



INTRODUCTION

Researchers are paying closer attention to nanofluid because of its unique physical characteristics and wide range of uses, particularly in the manufacturing, industrial, and biomedical sectors. Nanofluids are the most appropriate coolants in the aforementioned specific uses due to their increased heat conductivity. Choi and Eastman [1] introduced nanofluids to address the aforementioned significant concern. Nanofluids are defined as a blend of conventional fluids with Nanoscale particles (metals, metal oxides, etc.) that have superior heat transmission properties. Because nanofluids have noticeably better thermal conductivities, they function well as coolants in different zones. Computers, nuclear reactors, surgery, treatment of chronic illnesses, various microelectronic devices, cars, and transformers are a few examples of these application sectors [2-7]. Nagaraja et al. [8] expresses impact of conveying ternary hybrid nanofluid radiative flow in presence of aiding flow conditions by applying shooting algorithm. Influence of heat radiation and thermophoretic deposition by following RKF (Runge Kutta Fehlberg) technique has been reported by Karthik et al. [9] across wedge and shows that mass transfer rate declines because of enhancement in solid volume fraction. Reddy et al. [10] uses FEM (Finite Element Method) technique to study slip effects in presence of suction utilizing Al_2O_3 & TiO_2 hybrid nanoparticles and presented that with rise in volume fraction of Al_2O_3 & TiO_2 , temperature rises up. Asalekar et al. [11] discussed the influence of vegetable nanofluids induced by novel hybrid nanoparticles by utilizing ANN prediction. Mebarek-Oudina et al. [12] discussed the magnetite-water fluid flow. Sheikholeslami and Khalili [13] presented numerical simulation for spectral splitter induced by nanofluids. Jayadevamurthy et al. [14] studied the bioconvective flow induced by rotating disc utilizing unsteady fluid flow. Sephehrnia et al. [15] discussed dynamic viscosity & sensitivity analysis based on SiO_2 / *MWCNT*.

The extensive industrial and engineering uses of Casson fluids have drawn more attention to their study. All of these commonly used goods have one thing in common: they are indifferent to Newton's law of viscosity. As a result, these liquids are well known for not being Newtonian. When β is the Casson parameter, the Casson fluid has limiting features (non-Newtonian fluidity) that reflect infinite viscosity at zero shear stress $\beta \rightarrow 0$ and Newtonian viscosity at enormous stress $\beta \rightarrow \infty$. This is the unique quality that Casson fluid has. When shear tension and small shear strain exceed a threshold, the behavior of Casson fluid is similar to that of a flexible solid. Alqahtani et al. [16] utilizing HAM (Homotopy Analysis Method) algorithm to study impact of Al_2O_3 & *Cu* hybrid nanoparticles in presence of Darcy effects induced via exponential sheet. Puneeth et al. [17] studied influence of non-Newtonian nanofluid flow along with gyrotactic microorganisms flowing between diverging channels utilizing FEM & by applying similarity transformation. Akaje et al. [18] utilizing Spectral Collocation Method to analyze

analytically influence of chemical reaction & MHD Casson nano liquids and shows that with increase in Soret effects, concentration distribution rises up. Seethamahalakshmi et al. [19] reported impact of convection heating and slip flow induced by Maxwell nanofluid over porous surface.

The look at of the drift of electrically carrying out fluids in a regular or fluctuating magnetic Field (MF) is referred to as magnetohydrodynamics (MHD). Many uses for MHD have been discovered, including the transportation of subterranean species, improved oil recovery, medicine, biology, geothermal reservoirs, refrigeration systems, and encompassing power plants, among many more. Lund et al. [20] utilizing the bvp4c approach to study thermal radiation impact induced by Al_2O_3 - *Cu*/SA hybrid Casson nanofluids with MHD flow over permeable surface. Ali et al. [21] expressed impact of hydromagnetic flow in addition to thermal radiation induced via stretching surface and calculated results by utilizing Tecplot-360 software. Influence of activation energy in presence of MHD Casson nanofluid flow over exponential surface under the impact of Hall current by using MATLAB bvp4c package has been presented by Kumar et al. [22]. In recent years, MHD nanofluid flow has been addressed in [23, 24]. Gaseous modelling combustion utilizing species transport approach has been presented by Rajak et al. [25]. Rajak et al. [26] discussed diesel engine characteristics by following 3D CFD numerical approach.

This model garnered significant attention from scientists because of distinctive characteristics and considerable potential applications. It has diverse applications, encompassing power plants, refrigeration systems, medical science, and other fields. The goal of the current work is to investigate how chemical reactions affect the flow of free stream MHD nanofluids when heat convection occurs across a permeable surface. The study extensively analyzes and discusses the distinct behaviors of flow velocity, fluid temperature, and nanoparticle concentration in response to various critical physical parameters makes this research novel one. The dimensionless basic differential equation systems were computationally solved using the MATLAB software and the computational RKF technique by using the ODE45 solver. The current study's distinctive findings are beneficial and relevant for academic research as well as other fields.

MATHEMATICAL FORMULATION

The 3D model under consideration includes nanofluid MHD flow, heat production, and chemical reaction embedded in a permeable sheet with concentration and thermal Biot numbers (Fig. 1). Where a and b are constants, flow is constrained at $z \geq 0$ and positioned between stretching velocities $U_w = ax$ & $V_w = by$ at $z = 0$ at $z = 0$. Considered physical problem is analyzed with the below adopted assumptions:

- ❖ Free stream velocity flow
- ❖ Boundary layer Problem
- ❖ Reynolds number
- ❖ Heat radiation
- ❖ Thermal Diffusion

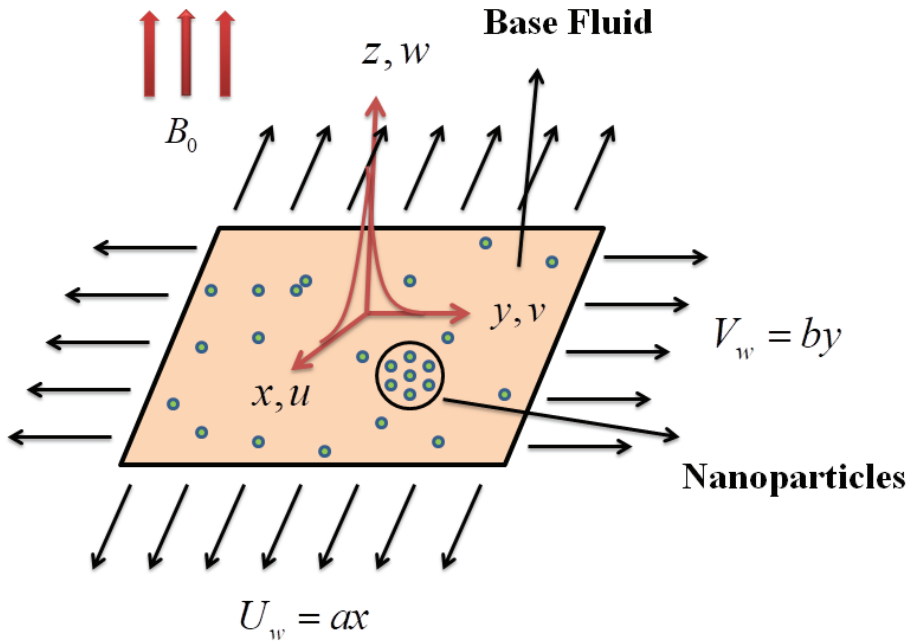


Figure 1. Physical diagram.

The considered governing equations are [2, 27, 28]:

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0 \tag{1}$$

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} = \nu \frac{\partial^2 u}{\partial z^2} + U_\infty \frac{\sigma B_0^2}{\rho} + U_\infty \frac{\partial U_\infty}{\partial z} - \left[\frac{\sigma B_0^2}{\rho} + \frac{\nu}{k_1} \left(1 + \frac{1}{\beta} \right) \right] u \tag{2}$$

$$u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} + w \frac{\partial v}{\partial z} = \nu \frac{\partial^2 v}{\partial z^2} + U_\infty \frac{\sigma B_0^2}{\rho} + U_\infty \frac{\partial U_\infty}{\partial z} - \left[\frac{\sigma B_0^2}{\rho} + \frac{\nu}{k_1} \left(1 + \frac{1}{\beta} \right) \right] v \tag{3}$$

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} + w \frac{\partial T}{\partial z} = \frac{k_1}{(\rho C_p)_f} \frac{\partial^2 T}{\partial z^2} + \frac{(\rho C_p)_p}{(\rho C_p)_f} \left[\frac{D_T}{T_\infty} \left(\frac{\partial T}{\partial z} \right)^2 + D_B \frac{\partial T}{\partial z} \frac{\partial C}{\partial z} \right] - \frac{1}{(\rho C_p)_f} \frac{\partial q_r}{\partial z} \tag{4}$$

$$u \frac{\partial C}{\partial x} + v \frac{\partial C}{\partial y} + w \frac{\partial C}{\partial z} = \frac{D_T}{T_\infty} \frac{\partial^2 T}{\partial z^2} + D_B \frac{\partial^2 C}{\partial z^2} - K_r (C - C_\infty) \tag{5}$$

Where u, v and w denotes the velocity components along x, y and z direction respectively. Also, σ denotes electrical conductivity, β denotes Casson fluid parameter, ν denotes kinematic viscosity, B_0 denotes magnetic field intensity,

ρ denotes density of fluid, U_∞ denotes stream velocity, k_1 denotes thermal conductivity, T denotes temperature, $(\rho C_p)_p$ denotes heat capacity at constant pressure, C denotes concentration, C_∞ denotes ambient concentration, D_T denotes thermophoretic diffusion coefficient, K_r denotes dimensionalized chemical reaction, $(\rho C_p)_f$ denotes heat capacity of the fluid, T_∞ denotes ambient temperature, D_B denotes Brownian diffusion coefficient..

Using similarity variables [29]:

$$\zeta = \sqrt{\frac{a}{\nu}} z, \quad \Theta(\zeta) = \frac{T - T_\infty}{T_w - T_\infty}, \quad \Phi(\zeta) = \frac{C - C_\infty}{C_w - C_\infty}, \quad u = axf'(\zeta), \tag{6}$$

$$v = byg'(\zeta) \text{ and } w = -\sqrt{av[f(\zeta) + cg(\zeta)]}$$

Where, ζ denotes similarity variables, a & b denotes constants, Θ denotes temperature distribution, Φ denotes concentration distribution, T_w & C_w are the temperature and concentration at wall serially and c denotes stretching ratio parameter.

Associated B.C's are:

$$u = U_w = ax, \quad v = V_w = by \text{ at } w = 0, \tag{7}$$

$$-k_f \left(\frac{\partial T}{\partial z} \right) = h_f (T_w - T), \quad -D_B \left(\frac{\partial T}{\partial z} \right) = h_s (C_w - C) \text{ at } z = 0$$

$$u \rightarrow 0, \quad v \rightarrow 0, \quad T \rightarrow T_\infty, \quad C \rightarrow C_\infty \text{ as } z \rightarrow \infty$$

Transformed D.E's are as follows:

$$\left(1 + \frac{1}{\beta} \right) f''' - f'^2 - M(f' - \lambda) + \lambda^2 + (f + cg)f'' - \left[M + PR \left(1 + \frac{1}{\beta} \right) \right] f' = 0 \tag{8}$$

$$\left(1 + \frac{1}{\beta}\right)g''' - cg'^2 - M(g' - \lambda) + \lambda^2 + (f + cg)g'' - \left[M + PR\left(1 + \frac{1}{\beta}\right)\right]g' = 0 \tag{9}$$

$$\theta'' + Pr\left[(f + cg)\theta' + Nb\theta'\phi' + Nt\theta'^2 + Q\theta\right] = 0 \tag{10}$$

$$\phi'' + LePr(f + cg)\phi' + \left(\frac{Nt}{Nb}\right)\theta'' - LePrCR\phi = 0 \tag{11}$$

Where, M denotes magnetic parameter, PR denotes permeability parameter, λ denotes free stream velocity, Le denotes Lewis number, Pr denotes Prandtl number, Nb denotes Brownian motion, CR denotes chemical reaction, Q denotes heat source parameter and Nt denotes thermophoresis parameter.

Reduced B.C's are:

$$\begin{aligned} f' &= 1, \quad g' = 1, \quad \theta'(\zeta) = -TB(1 - \theta(\zeta)), \\ \phi'(\zeta) &= -CB(1 - \phi(\zeta)), \\ f' &\rightarrow 0, \quad g' \rightarrow 0, \quad \theta \rightarrow 0, \quad \phi \rightarrow 0 \end{aligned} \tag{12}$$

Where, TB & CB denotes thermal and concentration Biot numbers respectively. Also non-dimensionalized fluid parameters are symbolically represented as follows:

$$\begin{aligned} \beta &= p \frac{\mu_B}{\rho_z} \sqrt{2\pi_c}, \quad M = \frac{\sigma B_0^2}{\alpha\rho}, \quad Pr = \frac{\nu\rho C_p}{k}, \\ Nb &= \frac{\tau D_B(C_w - C_\infty)}{\nu}, \quad Le = \frac{\alpha}{D_B}, \quad CB = \frac{h_s}{\sqrt{\frac{a}{\nu} D_B}}, \\ Nt &= \frac{\tau D_T(T_w - T_\infty)}{\nu T_\infty}, \quad TB = \frac{h_f}{\sqrt{\frac{a}{\nu} k_f}} \end{aligned} \tag{13}$$

Non-dimensionalized physical quantities are as follows:

$$\begin{aligned} Sh_x &= \frac{-x}{(C_w - C_\infty)} \left(\frac{\partial C}{\partial z}\right) \Big|_{z=0}, \quad Nu_x = \frac{-x}{(T_w - T_\infty)} \left(\frac{\partial T}{\partial z}\right) \Big|_{z=0}, \\ Cf_y &= \frac{\tau_{yz}}{\rho U_w^2}, \quad Cf_x = \frac{\tau_{xz}}{\rho U_w^2} \end{aligned} \tag{14}$$

$$\begin{aligned} Sh_x Re_x^{-1/2} &= -\phi'(0), \quad Nu_x Re_x^{-1/2} = -\theta'(0), \\ Cf_y Re_x^{1/2} &= \left(1 + \frac{1}{\beta}\right)g''(0), \quad Cf_x Re_x^{1/2} = \left(1 + \frac{1}{\beta}\right)f''(0), \end{aligned} \tag{15}$$

Here Re_x is local Reynolds number.

Numerical Scheme

The MATLAB R2014a ODE45 solver and the RKF method are used to mathematically handle the arrangement of D.E's (8)–(11) with B.C's (12) (Fig. 2). Next, ten first-order D.E.s are created from these circumstances as

$$\tilde{r}(1)' = \tilde{r}(2) \tag{16}$$

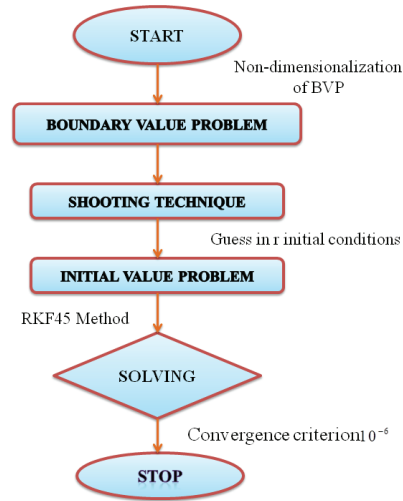


Figure 2. Numerical modelling flow chart.

$$\tilde{r}(2)' = \tilde{r}(3) \tag{17}$$

$$\begin{aligned} \tilde{r}(3)' &= \frac{\beta}{(1+\beta)} \left[\tilde{r}(2)^2 - \{\tilde{r}(1) + c\tilde{r}(4)\}\tilde{r}(3) \right. \\ &\quad \left. + M\tilde{r}(2) + K_1 \left(1 + \frac{1}{\beta}\right)\tilde{r}(2) \right] \end{aligned} \tag{18}$$

$$\tilde{r}(4)' = \tilde{r}(5) \tag{19}$$

$$\tilde{r}(5)' = \tilde{r}(6) \tag{20}$$

$$\begin{aligned} \tilde{r}(6)' &= \frac{\beta}{(1+\beta)} \left[c\tilde{r}(5)^2 - \{\tilde{r}(1) + c\tilde{r}(4)\}\tilde{r}(6) \right. \\ &\quad \left. + M\tilde{r}(5) + \beta K_1 \left(1 + \frac{1}{\beta}\right)\tilde{r}(5) \right] \end{aligned} \tag{21}$$

$$\tilde{r}(7)' = \tilde{r}(8) \tag{22}$$

$$\begin{aligned} \tilde{r}(8)' &= -Pr \left[\{\tilde{r}(1) + c\tilde{r}(4)\}\tilde{r}(8) + Nb\tilde{r}(8)\tilde{r}(10) \right. \\ &\quad \left. + Nt\tilde{r}(8)^2 \right] \end{aligned} \tag{23}$$

$$\tilde{r}(9)' = \tilde{r}(10) \tag{24}$$

$$\tilde{r}(10)' = -LePr \left\{ \tilde{r}(1) + c\tilde{r}(4) \right\} \tilde{r}(10) - \left(\frac{Nt}{Nb}\right)\tilde{r}(8)' \tag{25}$$

Where

$$\begin{aligned} f &= \tilde{r}(1), \quad f' = \tilde{r}(2), \quad f'' = \tilde{r}(3), \quad f''' = \tilde{r}(3)' \\ g &= \tilde{r}(4), \quad g' = \tilde{r}(5), \quad g'' = \tilde{r}(6), \quad g''' = \tilde{r}(6)' \\ \theta &= \tilde{r}(7), \quad \theta' = \tilde{r}(8), \quad \theta'' = \tilde{r}(8)' \\ \phi &= \tilde{r}(9), \quad \phi' = \tilde{r}(10), \quad \phi'' = \tilde{r}(10)' \end{aligned} \tag{26}$$

RESULTS AND DISCUSSION

In current analysis, results are compared along with residual error for different Pr as shown via Table 1. Table 2-4 presents values for $f''(0)$ & $g''(0)$, $-\theta'(0)$ and $\Phi'(0)$ for fixed entries of controlling fluid parameters as $\lambda = 0.1$ (Free stream velocity), $CB = 0.3$ (Concentration Biot number), $Q = 0.5$ (Heat generation parameter), $Cr = 0.6$ (Chemical reaction parameter), $c = 2.0$ (Stretching ratio parameter), $PR = 0.1$ (Permeability parameter), $\beta = 0.1$ (Casson fluid parameter), $M = 2.5$ (Magnetic parameter), $Pr = 0.73$ (Prandtl number), $Nb = 0.2$ (Brownian motion parameter), $Nt = 0.5$ (Thermophoresis parameter), $Le = 2.0$ (Lewis number), $TB = 0.1$ (Thermal Biot number).

The velocity distribution variation $g'(\zeta)$ against the parameter PR in the range of 0.05-0.10 is shown via Figure 3(a). This graph demonstrates how the velocity augmented somewhat when PR increases because there is more nano-fluid present farther from the boundary, indicating a

decrease in the thickness of the boundary layer and consequently, $g''(0)$ drops down from -0.819938652677649 to -0.849485482650904. The velocity distribution under the influence of λ ($0.10 \leq \lambda \leq 0.15$) is visualized in Figure 3(b). It was demonstrated that the velocity distribution and the free stream velocity parameter were closely proportional. As a result, when the free stream's velocity increases, the velocity distribution also increases and eventually decreases as it gets closer to the sheet's surface. The velocity distribution variation $g'(\zeta)$ against parameter M in the range of 0.1-0.5 as visualized in Figure 3(c). This graph demonstrates how the generated Lorentz drag force causes the velocity profile to fall gradually with little variation as the values of M increase. Furthermore, as Figure 3(c) illustrates, it has been observed that the width and magnitude of the boundary layer of $g'(\zeta)$ decrease with an increase in M and simultaneously $g''(0)$ declines from -0.574546600126926 to -0.628849145452216.

Table 1. A comparison for local Nusselt number with Hussain et al. [30], Wang [31] and Mabood et al. [32] along with residual error for different Pr

Pr	Hussain et al. [30]	Residual error	Wang [31]	Residual error	Mabood et al. [32]	Residual error	Present result
2	0.9114	0.0000	0.9114	0.0000	0.9114	0.0000	0.9114
20	3.3538	-0.0001	3.3539	0.0000	3.3539	0.0000	3.3539
70	6.4621	-0.0001	6.4622	0.0000	6.4622	0.0000	6.4622

Table 2. Values of $f''(0)$ & $g''(0)$ for PR ($0.05 \leq Pr \leq 0.10$), λ ($0.10 \leq \lambda \leq 0.15$) and M ($0.1 \leq M \leq 0.5$)

PR	λ	M	$f''(0)$	$g''(0)$
0.05	0.1	2.5	-0.777562025003942	-0.819938652677649
0.06	-	-	-0.784027644062844	-0.825920032046307
0.07	-	-	-0.790437876636590	-0.831865171691975
0.08	-	-	-0.796794192480612	-0.837774284907418
0.09	-	-	-0.803097995277020	-0.843647625792008
0.10	-	-	-0.809350626966072	-0.849485482650904
0.10	0.10	-	-0.809350626966072	-0.849485482650904
-	0.11	-	-0.806053793697922	-0.846480230407608
-	0.12	-	-0.802733021389691	-0.843455469273812
-	0.13	-	-0.799388321229795	-0.840411240406145
-	0.14	-	-0.796019704340752	-0.837347584780535
-	0.15	-	-0.792627182389335	-0.834264543020026
-	0.10	0.1	-0.511734517510804	-0.574546600126926
-	-	0.2	-0.527565224517534	-0.588618649457148
-	-	0.3	-0.542920574463810	-0.602341598180555
-	-	0.4	-0.557841369945768	-0.615743622955963
-	-	0.5	-0.572363162343344	-0.628849145452216

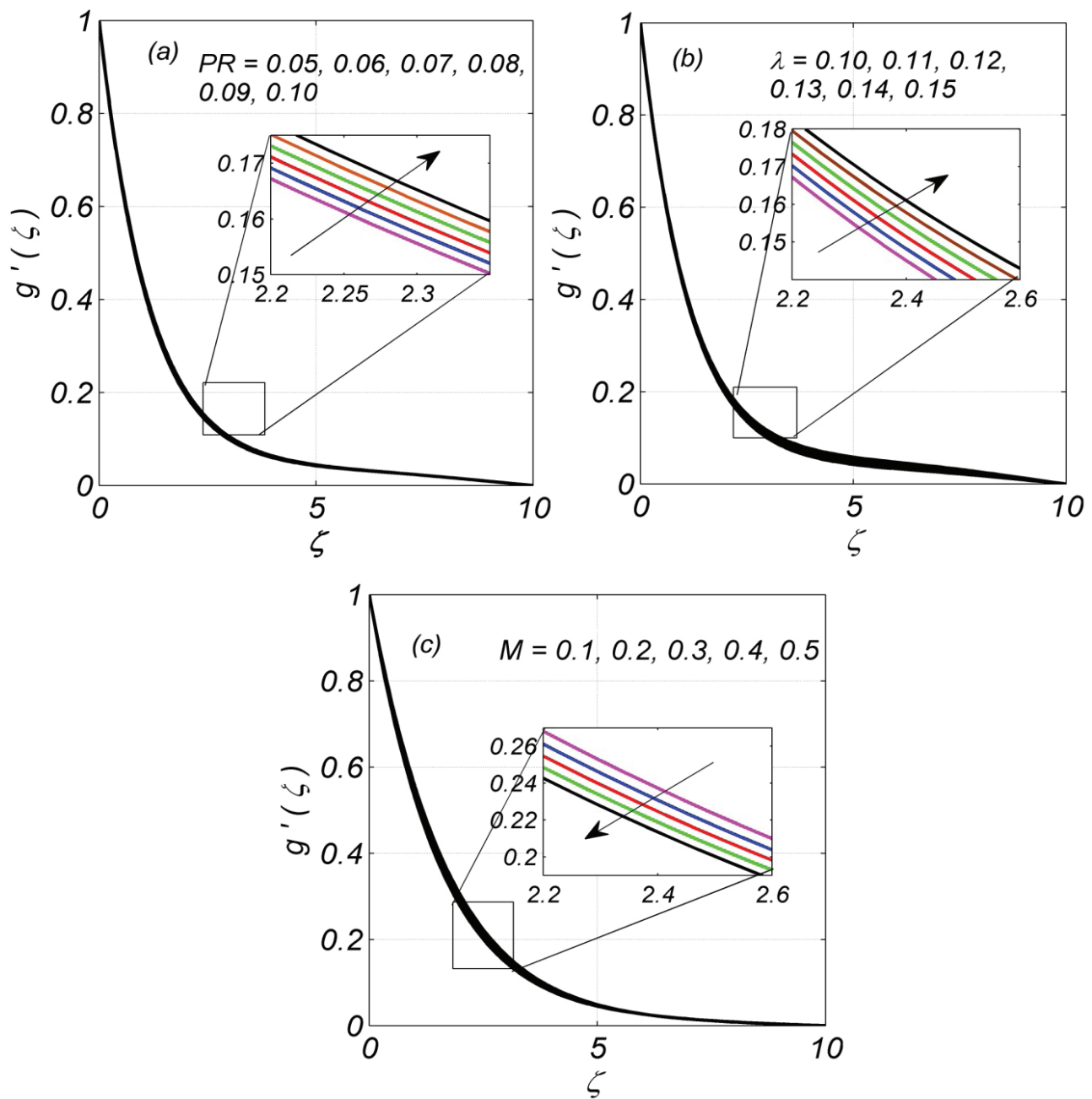


Figure 3. Velocity profile $g'(\xi)$ in direction of y -axis against (a) PR ($0.05 \leq PR \leq 0.10$), (b) λ ($0.10 \leq \lambda \leq 0.15$) and (c) M ($0.1 \leq M \leq 0.5$).

The temperature distribution's influence on the fluid parameters TB , c , Nb , Nt , Pr and Q are shown serially in Figures 4(a)-4(f). The temperature profile fluctuation against TB ($0.1 \leq TB \leq 0.9$) is explained in Figure 4(a), where it is observed that temperature and convection heating rising for higher TB . Additionally, graphs diverge for $0.0 \leq \zeta < 3.5$ (approximately), and then converge with $\zeta \rightarrow \infty$ beyond that. Furthermore, when TB fluctuates between 0.1 and 0.9, the Nusselt number decreases in the range of

-0.088541536369859 to -0.395288634252507 as shown on Table 3. The impact of stretching ratio parameter c ($2.0 \leq c \leq 10.0$) on the temperature profile is seen in Figure 4(b). It is noted that the temperature distribution decays with an increase in stretching ratio parameter c . Figure 4(c) shows the fluctuation in $\Theta(\zeta)$ for different levels of Nb . Plotting $\Theta(\zeta)$ against growing Nb ($1.0 \leq Nb \leq 9.0$) yields maximum values, as demonstrated. Higher Nb values physically result in thicker thermal barrier layers, which raise temperature.

Table 3. Values of $-\Theta'(0)$ for TB ($0.1 \leq TB \leq 0.9$), c ($2.0 \leq c \leq 10.0$), Nb ($1.0 \leq Nb \leq 9.0$), Nt ($2.0 \leq Nt \leq 10.0$), Pr ($0.2 \leq Pr \leq 1.0$) and Q ($0.50 \leq Q \leq 1.50$)

<i>TB</i>	<i>c</i>	<i>Nb</i>	<i>Nt</i>	<i>Pr</i>	<i>Q</i>	$-\Theta'(0)$
0.1	-	-	-	-	-	-0.088541536369859
0.3	-	-	-	-	-	-0.213904573511549
0.5	-	-	-	-	-	-0.296270136755862
0.7	-	-	-	-	-	-0.353538526151873
0.9	-	-	-	-	-	-0.395288634252507
-	2.0	-	-	-	-	-0.088541536376948
-	4.0	-	-	-	-	-0.092001343241164
-	6.0	-	-	-	-	-0.093483180597698
-	8.0	-	-	-	-	-0.094358344812766
-	10.0	-	-	-	-	-0.094953277965069
-	-	1.0	-	-	-	-0.087838005568556
-	-	3.0	-	-	-	-0.085846807677212
-	-	5.0	-	-	-	-0.083472797171521
-	-	7.0	-	-	-	-0.080643887962360
-	-	9.0	-	-	-	-0.077277950779695
-	-	-	2.0	-	-	-0.087728386458071
-	-	-	4.0	-	-	-0.086408477151171
-	-	-	6.0	-	-	-0.084677623243749
-	-	-	8.0	-	-	-0.082202020978397
-	-	-	10.0	-	-	-0.077875785228704
-	-	-	-	0.2	-	-0.073790700885929
-	-	-	-	0.4	-	-0.083609738138639
-	-	-	-	0.6	-	-0.087171204283452
-	-	-	-	0.8	-	-0.089119214400947
-	-	-	-	1.0	-	-0.090385039176517
-	-	-	-	-	0.50	-0.088541536376948
-	-	-	-	-	0.75	-0.086797493264815
-	-	-	-	-	1.00	-0.083979227817648
-	-	-	-	-	1.25	-0.078364642304093
-	-	-	-	-	1.50	-0.057225475769505

Similarly, as shown in Figure 4(d), raising the dimensionless thermophoresis parameter Nt ($2.0 \leq Nt \leq 10.0$) causes the thermophoretic force to become stronger. The impact of Nt on the dimensionless temperature profiles is shown in Figure 4(d). It has been noted that when Nt values rise, so does the temperature profile.

The relationship between Pr and $\Theta(\xi)$ is seen in Figure 4(e). The dimensionless curves indicate that at increased Pr ($0.2 \leq Pr \leq 1.0$), $\Theta(\xi)$ decreased. In actuality, there is an inverse relationship between thermal diffusivity and Prandtl number. Less thermal diffusivity results from an increase

in Pr , which causes a decline in the curves as visualized in Figure 4(e) and simultaneously Nusselt number drops down from -0.073790700885929 to -0.090385039176517 . The variance in $\Theta(\xi)$ for five distinct values of Q as 0.50, 0.75, 1.00, 1.20, and 1.50 is shown in Figure 4(f). When Q varies between 0.50 and 1.50, an increase in Q raises the fluid's temperature due to heat production via the heat source technique and the Nusselt number mounted in the range -0.088541536376948 to -0.057225475769505 .

The influence of concentration distribution against the fluid parameters CB , CR , Le , Nb , and Nt serially is shown in

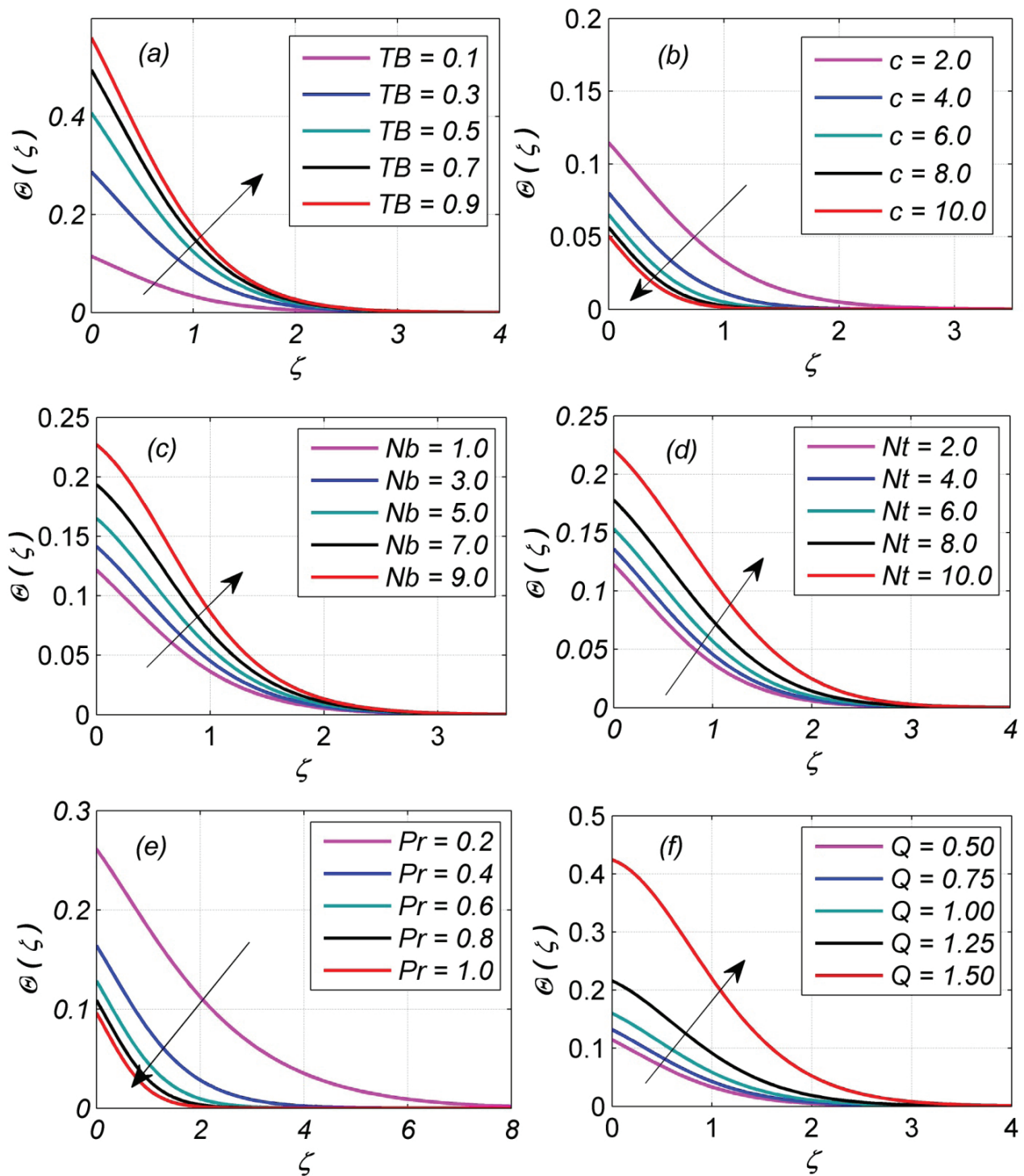


Figure 4. Temperature distribution against (a) TB ($0.1 \leq TB \leq 0.9$), (b) c ($2.0 \leq c \leq 10.0$), (c) Nb ($1.0 \leq Nb \leq 9.0$), (d) Nt ($2.0 \leq Nt \leq 10.0$), (e) Pr ($0.2 \leq Pr \leq 1.0$) and (f) Q ($0.50 \leq Q \leq 1.50$).

Figures 5(a)-5(e). Increase in concentration for greater CB ($0.2 \leq CB \leq 1.0$) values has been observed, is in fact visualized in Figure 5(a) and simultaneously, $-\Phi'(0)$ falls down from -0.172359090691536 to -0.612039859732770 . Influence of

chemical reaction CR ($0.5 \leq CR \leq 2.5$) on the distribution of nanoparticle concentrations is shown in Figure 5(b). It demonstrates that when the CR values increase, the concentration of nanoparticles drops. It takes place as a result

Table 4. Values of $-\Phi'(0)$ for CB ($0.2 \leq CB \leq 1.0$), CR ($0.5 \leq CR \leq 2.5$), Le ($1.5 \leq Le \leq 3.5$), Nb ($0.1 \leq Nb \leq 0.5$) and Nt ($1.0 \leq Nt \leq 5.0$)

<i>CB</i>	<i>CR</i>	<i>Le</i>	<i>Nb</i>	<i>Nt</i>	$-\Phi'(0)$
0.2	2.0	0.1	0.7	-	-0.172359090691536
0.4	-	-	-	-	-0.312804838685243
0.6	-	-	-	-	-0.429451162499494
0.8	-	-	-	-	-0.527875862277950
1.0	-	-	-	-	-0.612039859732770
-	0.5	-	-	-	-0.244440418143198
-	1.0	-	-	-	-0.251216249067726
-	1.5	-	-	-	-0.256160678776565
-	2.0	-	-	-	-0.259937729062749
-	2.5	-	-	-	-0.262925577508415
-	-	1.5	-	-	-0.236868031733801
-	-	2.0	-	-	-0.245990142265586
-	-	2.5	-	-	-0.252175904705804
-	-	3.0	-	-	-0.256708386246913
-	-	3.5	-	-	-0.260205066077814
-	-	-	0.1	-	-0.235663312096621
-	-	-	0.2	-	-0.245990142265586
-	-	-	0.3	-	-0.249433048679584
-	-	-	0.4	-	-0.251154979840411
-	-	-	0.5	-	-0.252188524353747
-	-	-	-	1.0	-0.236618805866993
-	-	-	-	2.0	-0.220094529005258
-	-	-	-	3.0	-0.206833023936196
-	-	-	-	4.0	-0.197284577613528
-	-	-	-	5.0	-0.192035907472882

of a decrease in molecule diffusivity with increasing CR and consequently, $-\Phi'(0)$ decreases from -0.244440418143198 to -0.262925577508415 . The effect of Lewis number Le ($1.5 \leq Le \leq 3.5$) on the distribution of nanoparticle concentrations is seen in Figure 5(c). It is observed that as Le values increase, the distribution of nanoparticle concentrations diminishes. Physically, a higher Lewis number causes the nanofluids mass diffusivity to decrease, which aids in lowering the concentration and, ultimately, the concentration of the nanoparticles. Figures 5(d) and 5(e) show concentration distribution for the greater values of the Nb ($0.1 \leq Nb \leq 0.5$) and Nt ($1.0 \leq Nt \leq 5.0$) respectively. It indicates that the concentration declines for higher Brownian motion parameter, whereas the thermophoresis parameter exhibits its obverse behavior. Furthermore, when Nb fluctuates between 0.1 and 0.5, the Sherwood number decreases in the range of -0.235663312096621 to -0.252188524353747 .

The skin friction coefficient is shown using contour plots against the computational fluid parameters TB & Pr , Nt & CB , Nt & Le , and Nt & Pr , respectively, in Figures 6(a)-6(d). Figure 6(a) elaborates the change in skin friction against thermal Biot numbers TB ($0.00 \leq TB \leq 1.50$) and Prandtl numbers Pr ($0.00 \leq Pr \leq 1.50$). This contour plot illustrates that skin friction increases as TB and Pr increases. The contour plot of skin friction across the thermophoresis parameter Nt ($0.00 \leq Nt \leq 1.50$) and concentration Biot number CB ($0.00 \leq CB \leq 2.50$) as visualized in Figure 6(b), and it indicates that skin friction increases as both Nt and CB increase. Similarly, as can be seen in Figures 6(c), the contour plots provided via them demonstrate that skin friction increased with larger Nt & Le and Figure 6(d) shows skin friction increases when Nt ($0.00 \leq Nt \leq 1.50$) rises and Pr ($0.00 \leq Pr \leq 1.50$) falls.

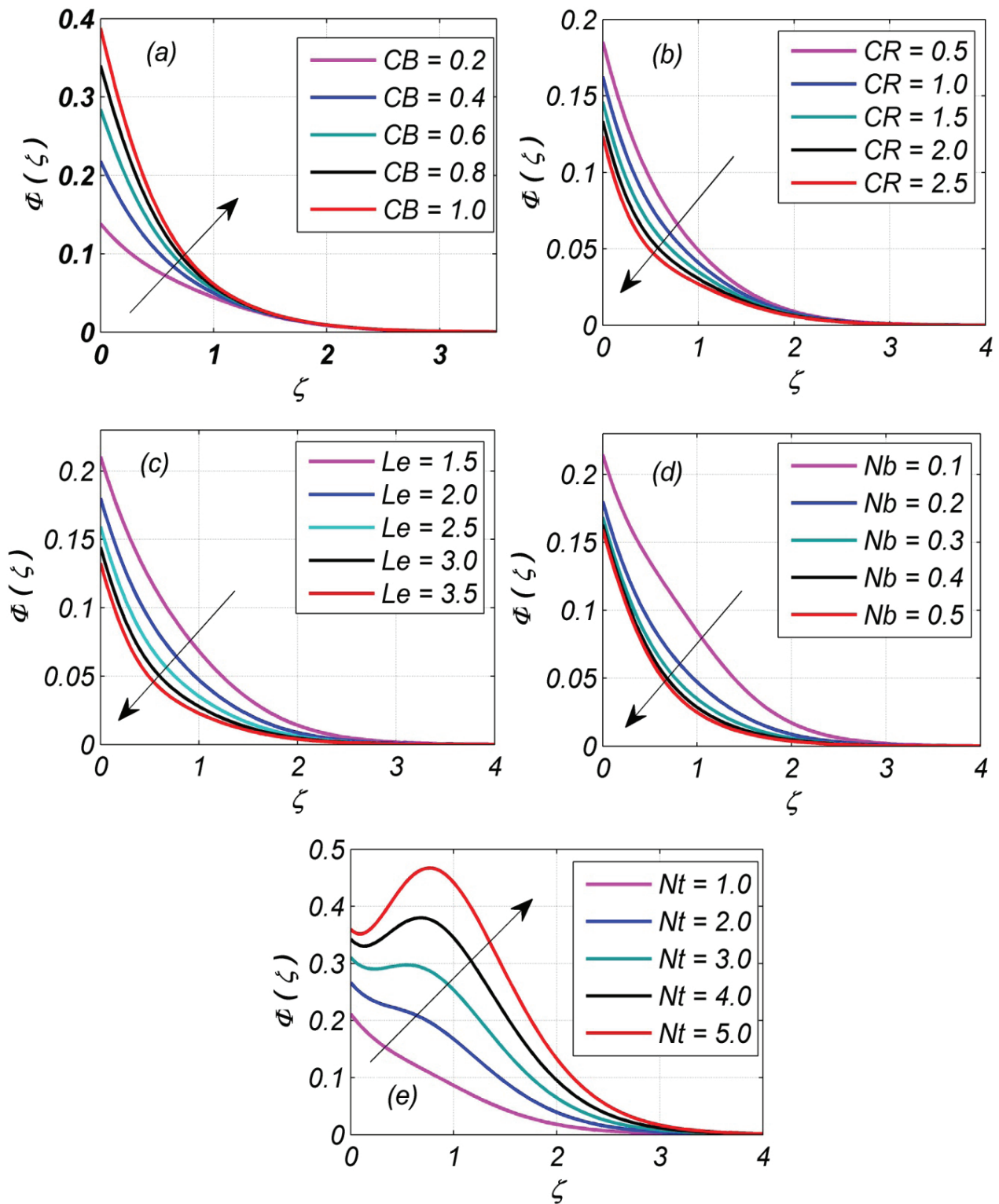


Figure 5. Concentration distribution against (a) CB ($0.2 \leq CB \leq 1.0$), (b) CR ($0.5 \leq CR \leq 2.5$), (c) Le ($1.5 \leq Le \leq 3.5$), (d) Nb ($0.1 \leq Nb \leq 0.5$) and (e) Nt ($1.0 \leq Nt \leq 5.0$).

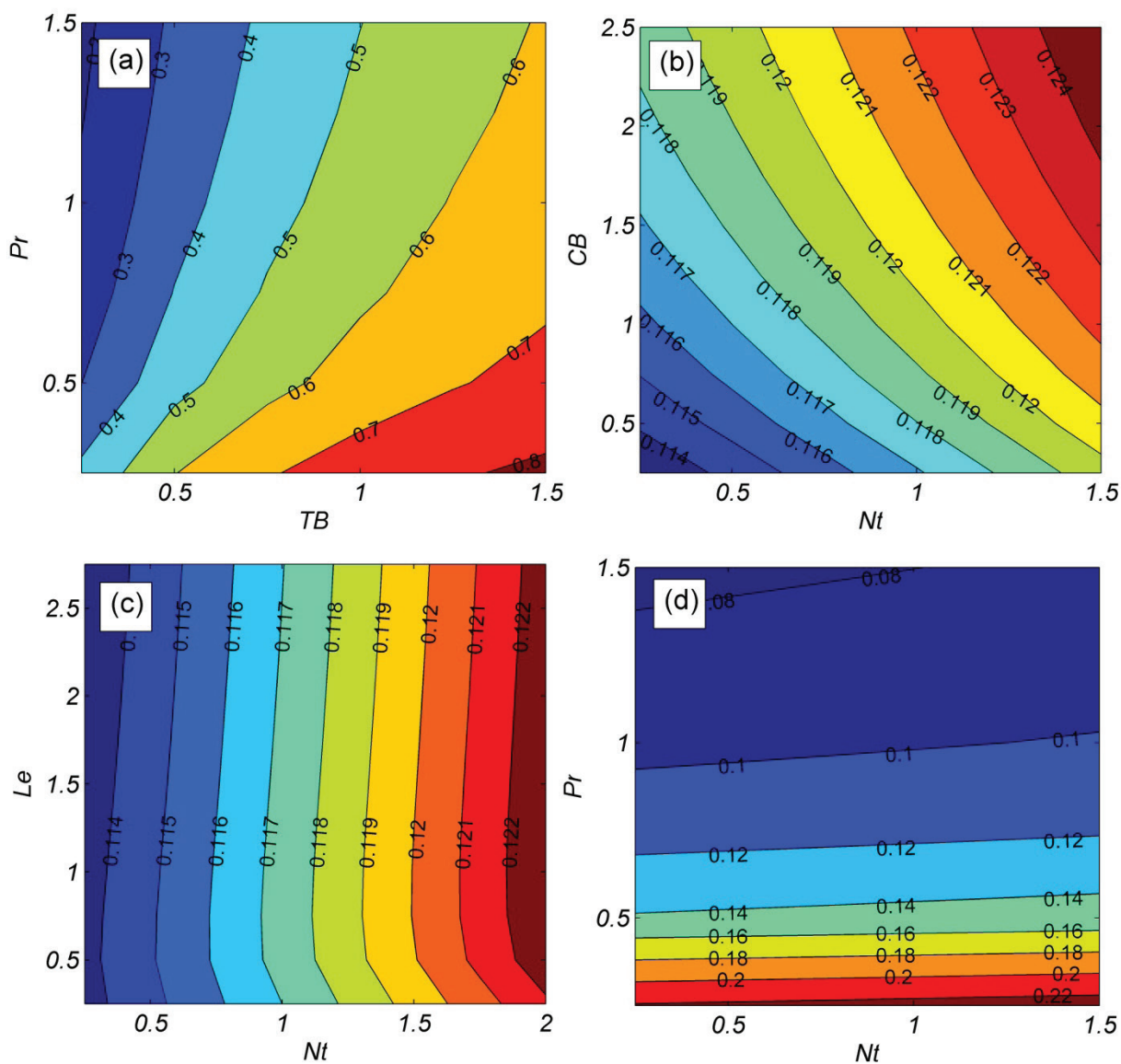


Figure 6. Skin friction coefficient against (a) TB & Pr , (b) Nt & CB , (c) Nt & Le and (d) Nt & Pr .

CONCLUSION

The transformation of partial differential equations into ordinary differential equations is accomplished by the use of similarity conversion. Final results include the temperature distribution, volume fraction of nanoparticles, Magnetohydrodynamics Casson nanofluid flow and the importance of Biot numbers. Final outcomes are as follows:

1. Intensification in concentration has been noticed out for higher concentration Biot number while concentration falls down for greater chemical reaction, Lewis number as well as Brownian motion.
2. Augmentation in the values of thermal Biot number, Brownian motion, thermophoresis and heat generation helps to increase temperature distribution. On

the other hand, temperature declines with the increase in values of stretching ratio parameter and Prandtl number.

3. Higher stretching ratio parameter ranging from 2.0-10.0 leads to fall down heat transfer rate by 7.24%.
 4. With rise in the values of Prandtl number from 0.2 to 1.0, heat transfer rate falls down by 22.37%.
 5. Velocity declines against higher magnetic parameter due to Lorentz drag force.
 6. Inclination in velocity is observed for greater permeability parameter and free stream velocity parameter.
 7. Skin friction coefficient rises up with simultaneous augmentation in thermal Biot number and Prandtl number.
- The results of this study are useful for controlling the heat transfer rate and fluid velocity in various industrial

applications, biochemical systems, and manufacturing processes so that the final product satisfies quality requirements. Current study can be extended for various non-Newtonian fluids by utilizing entropy generation, porous medium, joule heating, etc.

NOMENCLATURE

x, y, z	Cartesian Coordinates
u, v, w	Velocity Components
ν	Kinematic Viscosity
U_∞	Free Stream
σ	Electrical Conductivity
B_0	Magnetic Field Intensity
ρ	Density
k_1	Thermal Conductivity
β	Casson Fluid
T	Temperature
$(\rho C_p)_p$	Specific Heat at Constant Pressure
D_T	Thermophoretic Diffusion Coefficient
T_∞	Ambient Temperature
D_B	Brownian Diffusion Coefficient
C	Concentration
K_r	Chemical Reaction
C_∞	Ambient Concentration
ζ	Similarity Variable
a, b	Constants
Θ	Dimensionless Temperature
T_w	Wall Temperature
Φ	Dimensionless Concentration
C_w	Wall Concentration
f	Dimensionless Velocity in x -direction
g	Dimensionless Velocity in y -direction
M	Magnetic Parameter
λ	Free Stream Velocity
PR	Permeability Parameter
Pr	Prandtl Number
Nb	Brownian Motion
Nt	Thermophoresis Parameter
Q	Heat Generation
Le	Lewis Number
CR	Dimensionless Chemical Reaction
TB	Thermal Biot Number
CB	Concentration Biot Number
Sh_x	Sherwood Number
Nu_x	Nusselt Number
Cf_y	Skin Friction in y -direction
Cf_x	Skin Friction in x -direction
Re_x	Reynolds Number
c	Stretching Ratio Parameter
$(\rho C_p)_f$	Heat capacity of the fluid

Abbreviations

O.D.E's	Ordinary Differential Equations
P.D.E's	Partial Differential Equations
MWCNT	Multi Walled Carbon Nanotubes

CFD Computational Fluid Dynamics

MHD Magnetohydrodynamics

RKF45 Runge Kutta Fehlberg forth-fifth

AUTHORSHIP CONTRIBUTIONS

Authors equally contributed to this work.

DATA AVAILABILITY STATEMENT

The authors confirm that the data that supports the findings of this study are available within the article. Raw data that support the finding of this study are available from the corresponding author, upon reasonable request.

CONFLICT OF INTEREST

The authors declared no potential conflicts of interest with respect to the research, authorship, and/or publication of this article.

ETHICS

There are no ethical issues with the publication of this manuscript.

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