



## Research Article

# Green synthesis of BT-Fe<sub>3</sub>O<sub>4</sub> nanocomposite using *Camellia sinensis* leaves extract: Characterization, NPEO adsorption experiments, isotherms, and kinetics

Pınar BELİBAĞLI<sup>1</sup>, Yağmur UYSAL<sup>1,\*</sup>

<sup>1</sup>Mersin University, Department of Environmental Engineering, Mersin, Turkey

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## ABSTRACT

In this study, Black Tea-Fe<sub>3</sub>O<sub>4</sub> (BT-Fe<sub>3</sub>O<sub>4</sub>) magnetite nanocomposites was synthesized from extract of black tea (*BT-Camellia sinensis*) leaves with an eco-friendly method, and used to investigate nonylphenol ethoxylate (NPEO) removal potential from water. The results of the characterization determination studies performed on the adsorbent revealed that the herbal extract obtained from black tea leaves successfully covered the surface of magnetite (Fe<sub>3</sub>O<sub>4</sub>) nanoparticles. Batch tests were carried out to define the action of BT-Fe<sub>3</sub>O<sub>4</sub> dose, initial NPEO concentration, pH and contact time on the adsorption attitude of the BT-Fe<sub>3</sub>O<sub>4</sub>. Adsorption isotherms and kinetics were described by a Freundlich isotherm model and pseudo-second-order kinetic model. The experimental results showed that maximum adsorption efficiency of NPEO (%73.45) occurred the optimal pH value of 7.0, NPEO concentration of 10 mg/L, BT-Fe<sub>3</sub>O<sub>4</sub> dose of 1g/L, and contact time of 60 minutes. The results of the study have shown that BT-Fe<sub>3</sub>O<sub>4</sub> particles have promising applicability in the removal of NPEO from aqueous media by adsorption method as an environmentally friendly and low-cost alternative adsorbent with rapid separation ability for wastewater treatment.

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## INTRODUCTION

According to results of the research conducted by the World Wide Fund for Nature (WWF) and Eurostat, worldwide chemical production has been increasing

exponentially since 1903. In 2017, 97.8 million tons of these chemicals were reported to be harmful to the environment and health [1]. Nonylphenol ethoxylates (NPEO) are

### \*Corresponding author.

\*E-mail address: [yagmuruyisal@gmail.com](mailto:yagmuruyisal@gmail.com)

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produced approx. 400,000 tons of year worldwide. NPEOs are one of the commonly used nonionic surfactants, and consist of a hydrophobic structure with a hydroxyl group, a phenol ring and a linear nonyl chain in the para position [2]. The increasing industrial demand for NPEOs and their usage in anthropogenic activities have increased their emergence as a contaminant in drainage mud and garbage dump sites due to waste evacuation, water treatment plants, and random dumping [3, 4].

NPEO has been detected in streams at concentration switching from 2.5 to 97.6  $\mu\text{g/L}$  [5] and risk coefficient greater than 1.0 indicating that may pose significant ecotoxicological risks [6]. Nonylphenol (NP) in the medium originates from the degradation of nonylphenol ethoxylates (NPEOs) [7]. According to previous studies, the average NP concentration in sewage sludge used for soil improvement was determined as 24.907 mg/kg [8]. It has been determined that NP concentration in wastewater treatment plants is measured as 0.79  $\mu\text{g/L}$  and this value can reach up to 0.1-1.2 mg/L around contaminated rivers and septic systems [9]. Various studies have shown that NPs can mimic natural estrogens with the estrogen receptor, thus inhibiting the activity of the hormone, bioaccumulating in aquatic organisms, altering the endogenous levels of steroids, diabetes, reproductive system, and is associated with obesity [4, 10-13]. Consequently, numerous countries have restricted the use of NPEO surface-active agents [14]. The current policy on NP in the European Commission is to ban its use within the European Union through the 2003/53/EC Directive. [15].

Many technologies such as biological, physical, and biotechnological methods have been applied to separate or treat NPEOs from wastewater. Combined methods for adsorption and enhanced oxidation processes (ie. photocatalysis) are attractive as they get the benefit of synergistic impacts [2, 16]. It has been viewed that adsorption is one of the very effective, economic, and effortless methods for contaminant removal. However, the transmission of complexes into the solid phase owing to adsorption can beget a secondary contaminant in water. This issue could be intercepted by adopting an alternative way such as nanomaterials based photo-catalysis [17-19]. Nevertheless, there are few studies on the synthesis of nanomaterials that meet all these criteria. Therefore, green synthesis methods that are environmentally, economically, and technically feasible are needed instead of traditional methods [20]. Nanomaterials produced using herbal phytochemicals notably decrease environmental contaminants, aid economically viable and sustainable neat and green chemistry technologies [21].

The selection of green synthesis routes may conduct significant benefits over the traditional process. For example, traditional processes tend to produce waste (liquid or solid), which often signals the use of costly chemicals and additional investments in the treatment of these pollutants [22-25]. Plant-based nanomaterial synthesis is preferred as

it can be produced from a large number of different natural substances, and powerful biomolecular reducing agents can be obtained from a variety of plants [26]. It has been reported that plants contain a wide variety of antioxidants and secondary metabolites, and these biomolecules work in harmony to inhibit cellular components [27, 28]. Plant extracts contain reducing and stabilizing agents for the synthesis of magnetite nanoparticles such as phenols, carboxylic acid, and amino acids [29, 30]. Black teas within the *Camellia sinensis* family grow in temperate and tropical areas. The rich source of polyphenols in the structure of black tea leaves acts as a reducing agent in the synthesis of metal nanoparticles [31].

The fundamental goal of this paper is to investigate the potential of green synthesized BT- $\text{Fe}_3\text{O}_4$  composite to adsorb environmentally harmful nonylphenol ethoxylates as adsorbent material. The novelty of this study is to obtain a new magnetite composite material using Black Tea leaves (an eco-friendly stabilizing matter for the synthesis of magnetite materials) so combine these properties in a single substance. Also to our knowledge, preparation, and application of BT- $\text{Fe}_3\text{O}_4$  for NPEO removal in solutions have not yet been studied. Experimental studies were conducted as follows: (1) Characterization of green synthesized BT- $\text{Fe}_3\text{O}_4$  to control the chemical species on the surface of the nanomaterial and the changes in its structure before and after NP adsorption; (2) Batch adsorption experiments performed to optimize various parameters such as pH, nano-dose, initial NPEO concentration and contact time; and (3) Kinetic studies to examine the stability of the adsorption isotherm and the adsorption process.

## MATERIAL AND METHODS

### MATERIALS

NPEO stock solution (1000 mg/L) was prepared from nonylphenol ethoxylate (Acar Chemistry). All chemicals such as  $\text{NH}_4\text{OH}$ ,  $\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$ ,  $\text{FeCl}_2 \cdot 4\text{H}_2\text{O}$ , HCl and NaOH (Merck) used in the synthesis of magnetite nano-composites and required for experiments were analytical reagents.

### Green Synthesis of Magnetite Nanomaterials From Black Tea (*Camellia Sinensis*) Extract

First, the purchased black tea leaves were washed several times with distilled water, to remove dust and dirt and dried. Then tea extract was prepared by boiling 30g/0.5L of the leaves of that plant at 80°C for 1h. After precipitation for 1 h, the extract was filtered. Then a magnetite nanoparticle ( $\text{Fe}_3\text{O}_4$ ) solution was prepared by adding 6.1278 g of solid  $\text{FeCl}_3 \cdot 4\text{H}_2\text{O}$  and 3.0121 g of solid  $\text{FeCl}_2 \cdot 6\text{H}_2\text{O}$  into 100 mL of deionized water under  $\text{N}_2$  medium. When the solution temperature reached to 85°C, 25 mL of 25% purity ammonia ( $\text{NH}_3$ ) solution was stirred for 2 min. to

be a homogeneous mixture. Then tea extract was added and the reaction was stirring out in nitrogen for during 30 min and cooled to room temperature. At this time, a black precipitate formed, evidencing the formation of BT-Fe<sub>3</sub>O<sub>4</sub> particles. The BT-Fe<sub>3</sub>O<sub>4</sub> nanoparticles formed were washed several times with distilled water and separated with neodymium magnet [32, 33].

### Instrumental Analyses

High-performance liquid chromatography (HPLC-Shimadzu LC-20AD) equipped with a fluorescence detector was used for measuring of NPEO concentrations. The morphology and size of the resulted BT-Fe<sub>3</sub>O<sub>4</sub> particles were characterized by Field Emission Scanning Electron Microscopy (FE-SEM). Fourier Transformed Infrared Spectroscopy (FT-IR) was realized by FT-IR-410.

### Batch Studies

Batch studies were performed in an orbital shaker with a constant speed of 200 rpm in 100mL flasks. After that, NPEO solutions were centrifuged (4000 rpm), and the solutions of NPEO in the supernatant solutions were analyzed by using an HPLC. The main process parameters considered were pH (3.0, 5.0, 7.0, 9.0, 11.0), initial NPEO concentration (10, 20, 40, 60, 80 mg/L), nanoparticle dose (1, 2, 4, 6, 8 g/L), and contact time (10, 20, 40, 60, 90 min). For the accuracy of the results obtained, the experiments were repeated twice and their average result reported.

The removal percentage (%) of NPEO was calculated for as follows each run by using Equation (1)

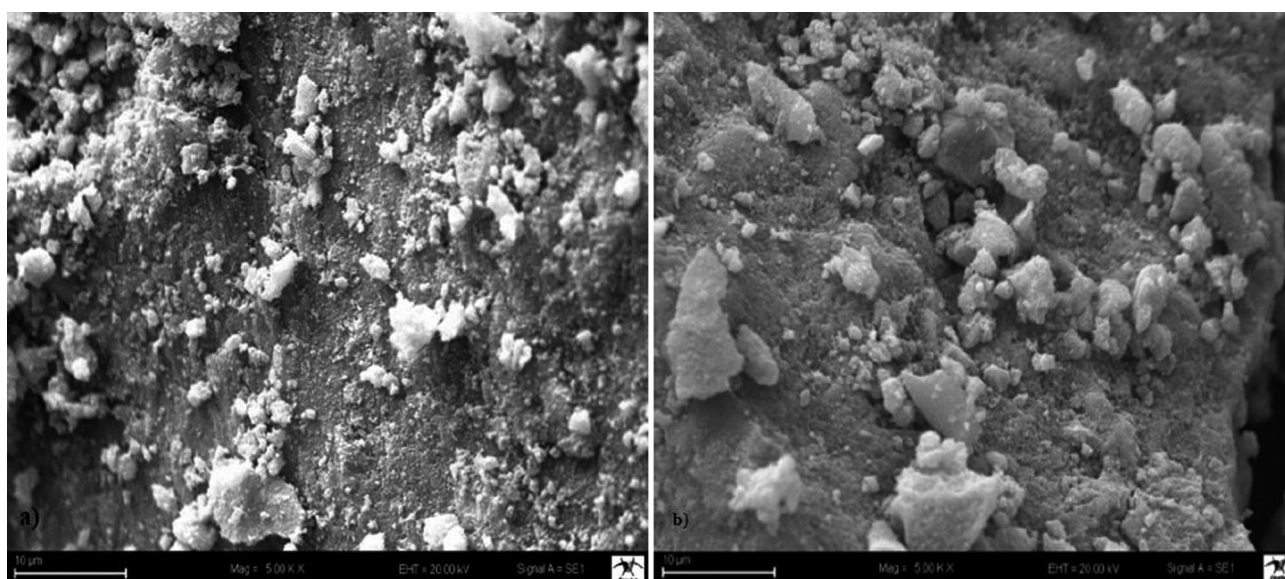
$$\% \text{ removal} = \frac{C_0 - C_e}{C_e} \times 100 \quad (1)$$

where C<sub>0</sub> (mg/L) and C<sub>e</sub> (mg/L) are the initial and balance concentrations of NPEO.

## RESULTS AND DISCUSSION STRUCTURE ANALYSIS OF BT-Fe<sub>3</sub>O<sub>4</sub>

SEM surface analyses of the BT-Fe<sub>3</sub>O<sub>4</sub> particles before and after the adsorption were used to identify synthesized particles, and were shown in Fig. 1(a-b). Before the adsorption process, nanocomposite particles had an irregular and rough surface (Fig 1a). In Figure 1b, it was observed that after adsorption of NPEO removal, the nanoparticles generally exhibited rough surface morphology and flocculation was dominant.

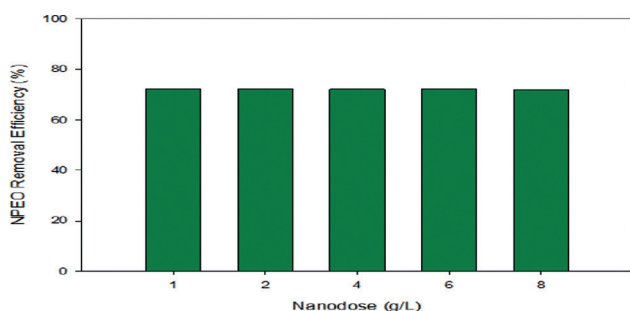
The FTIR spectrum of the nanoparticles produced was also shown in Fig. 2. For raw Fe<sub>3</sub>O<sub>4</sub> spectrum, the peaks at 1593.15 cm<sup>-1</sup> and 549.93 cm<sup>-1</sup> belonged to the C=C stretching and Fe stretching vibrations, respectively [34]. Before the adsorption process, for BT-Fe<sub>3</sub>O<sub>4</sub>, the peaks at 3126.37-2989.71 cm<sup>-1</sup> correspond to the stretching vibration of C-H (aliphatic) bending. The peaks at 1605.50 and 1401.63 cm<sup>-1</sup> show C=C (aromatic), and C-N bonds, respectively. The peak at 1060.15 cm<sup>-1</sup> corresponds to C-O bonds. As shown in Fig. 2, the adsorption peaks at 549.93 cm<sup>-1</sup>, 1060.15 cm<sup>-1</sup> and 1401.63 cm<sup>-1</sup> were related with the Fe<sub>3</sub>O<sub>4</sub> nanoparticles coated with black tea. After the adsorption process, the peak at 3369.84 cm<sup>-1</sup> for BT-Fe<sub>3</sub>O<sub>4</sub> related to the tension vibration of O-H.



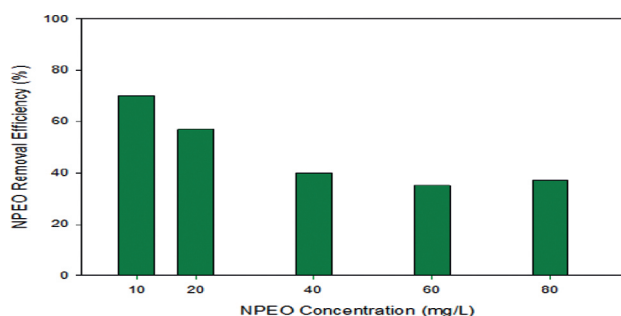
**Figure 1.** SEM analyses of BT-Fe<sub>3</sub>O<sub>4</sub> before (a) and after adsorption (b) with adsorbed NPEO.



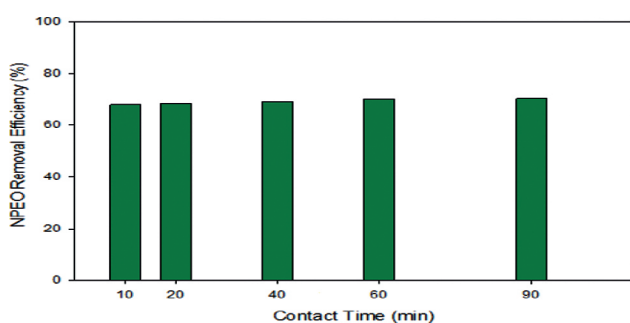




**Figure 4.** BT-Fe<sub>3</sub>O<sub>4</sub> on NPEO treatment. (pH: 7.0, NPEO Concentration: 20 mg/L, T: 25°C)



**Figure 5.** NPEO concentration on NPEO treatment. (pH: 7.0, BT-Fe<sub>3</sub>O<sub>4</sub> quantity: 1g/L, T: 25°C)



**Figure 6.** Contact time on NPEO treatment. (pH: 7.0, BT-Fe<sub>3</sub>O<sub>4</sub> quantity: 1g/L, NPEO Concentration: 10 mg/L, T: 25°C)

### Effect of NPEO Concentrations on the Process

The effect of initial NPEO concentrations on the treatment process of NPEO was shown in Fig.5. Figure 5 showed that the increasing of NPEO concentrations induce a notable reduction in the treatment efficiency of BT-Fe<sub>3</sub>O<sub>4</sub>. This behavior is due to the filling of functional groups on the BT-Fe<sub>3</sub>O<sub>4</sub> surface due to the increase in the initial NPEO concentrations of BT-Fe<sub>3</sub>O<sub>4</sub> particles [41]. While removal efficiency was achieved at 70% values at 10 mg/L NPEO concentration, removal efficiency continued at 40% at concentrations where the NPEO concentration in the environment increased to 40 mg/L and above. This shows that this adsorbent can be used efficiently for wastewater with NPEO concentrations of 10 mg/L or less, depending on the desired treatment efficiency.

### Effect of Time on the Process

The impact of time on the removal efficiency of NPEO by BT-Fe<sub>3</sub>O<sub>4</sub> was investigated at various reaction times (10–90 min). Figure 6 shows that removal efficiency does not change significantly with time. A removal efficiency in the range of 60–70% has been achieved in the first 10 minutes

from the start of the adsorption. This yield increased slightly up to 60 minutes, and did not change significantly when the time was extended to 90 minutes. This revealed that the adsorbent reached saturation in a very short time. The retention time reaching equilibrium in 60 minutes can be explained by filling all active sites of BT-Fe<sub>3</sub>O<sub>4</sub> particles with NPEO [42].

The adsorption capacity of BT-Fe<sub>3</sub>O<sub>4</sub> for NPEO species was compared with adsorbents previously reported (Table 1). In general, the BT-Fe<sub>3</sub>O<sub>4</sub> nanocomposites have exhibiting faster equilibrium and nearly the same adsorption efficiency than almost all listed adsorbents. At the same time, the presence of the black tea structure together with the magnetic properties of the adsorbent reveals that an environmentally friendly, low-cost BT-Fe<sub>3</sub>O<sub>4</sub> adsorbent with fast separation capability can be used as a promising solution for NPEO adsorption.

### ISOTHERM MODELS

Isotherms studies are a useful tool to forecast the adsorbent effectiveness to removal a given pollutant from polluted water/wastewater. In order to define the model of NPEO removal on the BT-Fe<sub>3</sub>O<sub>4</sub>, isotherms were determined by exposing various doses of the adsorbent. The other affecting factors were kept constant. The parameters and correlation coefficients (R<sup>2</sup>) were summarized in Table 2 and Figure 7 (a, b, c, d). According to the fixed parameters shown in Table 1, the values of n and R<sub>L</sub> less than 1.0 showed that NPEO adsorption was positive. The results showed that the degree of fit for the Freundlich model was higher than that for the Harkins-Jura model.

### KINETIC MODELS

Kinetic studies are significant for the estimate of optimum conditions in the full-scale adsorption processes [49]. Three different kinetic models were used to determine the time-dependent variation of NPEO adsorption on BT-Fe<sub>3</sub>O<sub>4</sub> and its adsorption rate. In order to study the mechanism of

**Table 1.** Comparison of the maximum efficiency and adsorption capacities of NPEO on various adsorbents

| Adsorbent  | Optimal conditions   | Adsorption capacity or removal efficiency   | Ref.       |
|--|--|---|------------|
| PAMAM-MNP<br>(polyamidoamine magnetite nanoparticles)              | NPEO: -<br>pH: 7.0<br>Contact Time: 60 min<br>Temp.: 30°C            | Distilled water: 70%<br>Drinking water: 67%<br>Well water: 63%<br>Treated wastewater: 65% | [43]       |
| Fe <sub>3</sub> O <sub>4</sub> /AC<br>(magnetite-activated carbon) | NPEO: 1–5 mg/L<br>pH: 3.0<br>Contact Time: 30 min<br>Temp. 25°C      | 73.3%   | [44]       |
| Fly-ash-cenospheres/Fe <sub>3</sub> O <sub>4</sub>                 | NP: 2mg/L<br>pH: 6.0<br>Contact Time: 200 min<br>Temp.: 25°C         | 438.8 mg/g  | [45]       |
| Mg-Al-CO <sub>3</sub>  | NP: <3 mg/L<br>pH: 7.0–9.0<br>Contact Time: 10 min<br>Temp.: Ambient | 88–93%  | [46]       |
| WO <sub>3</sub> /TNAs<br>(Tungsten trioxide/Nanotube arrays)       | NP: 2mg/L<br>pH: 6.5–7.5<br>Contact Time: 120 min.<br>Temp.: Ambient | > 97%   | [47]       |
| Pectin-Fe <sub>3</sub> O <sub>4</sub>                              | NPEO: 20 mg/L<br>pH:7<br>Contact Time: 60 min.                       | 62%   | [48]       |
| BT-Fe <sub>3</sub> O <sub>4</sub>                                  | NPEO: 10 mg/L<br>pH: 7.0<br>Contact Time: 60 min<br>Temp.: Ambient   | 73.3%   | This Study |

**Table 2.** The isotherm models and their constants

| Langmuir Model                                       | Freundlich Model   |
|--|--|
| $\frac{1}{q_e} = \frac{1}{bq_m C_e} + \frac{1}{q_m}$ | $\ln q_e = \ln K_f + \frac{1}{n} \ln C_e$  |
| Q (mg/g)   | K <sub>f</sub> (mg/g)(L/mg <sup>1/n</sup> )                                      |
| b (L/mg)   | n  |
| R <sub>L</sub>                                       | R <sup>2</sup>   |
| R <sup>2</sup>                                       |  |
| Tempkin Model  | Harkins-Jura Model   |
| $q_e = \frac{R.T}{b_T} \cdot \ln(A_T \cdot C_e)$     | $\frac{1}{q_e^2} = \left(\frac{B}{A}\right) - \left(\frac{1}{A}\right) \log C_e$ |
| B <sub>1</sub>                                       | A  |
| K <sub>T</sub> (L/g)                                 | B  |
| R <sup>2</sup>                                       | R <sub>2</sub>   |

q<sub>e</sub>: amount adsorbed, b: Langmuir constant, C<sub>e</sub>: equilibrium concentration q<sub>m</sub>: monolayer adsorption capacity, K<sub>f</sub> and n: Freundlich constants, R: constant, T: temperature, b<sub>T</sub> and A<sub>T</sub>: Tempkin isotherm constant, A and B: Harkins-Jura constants.

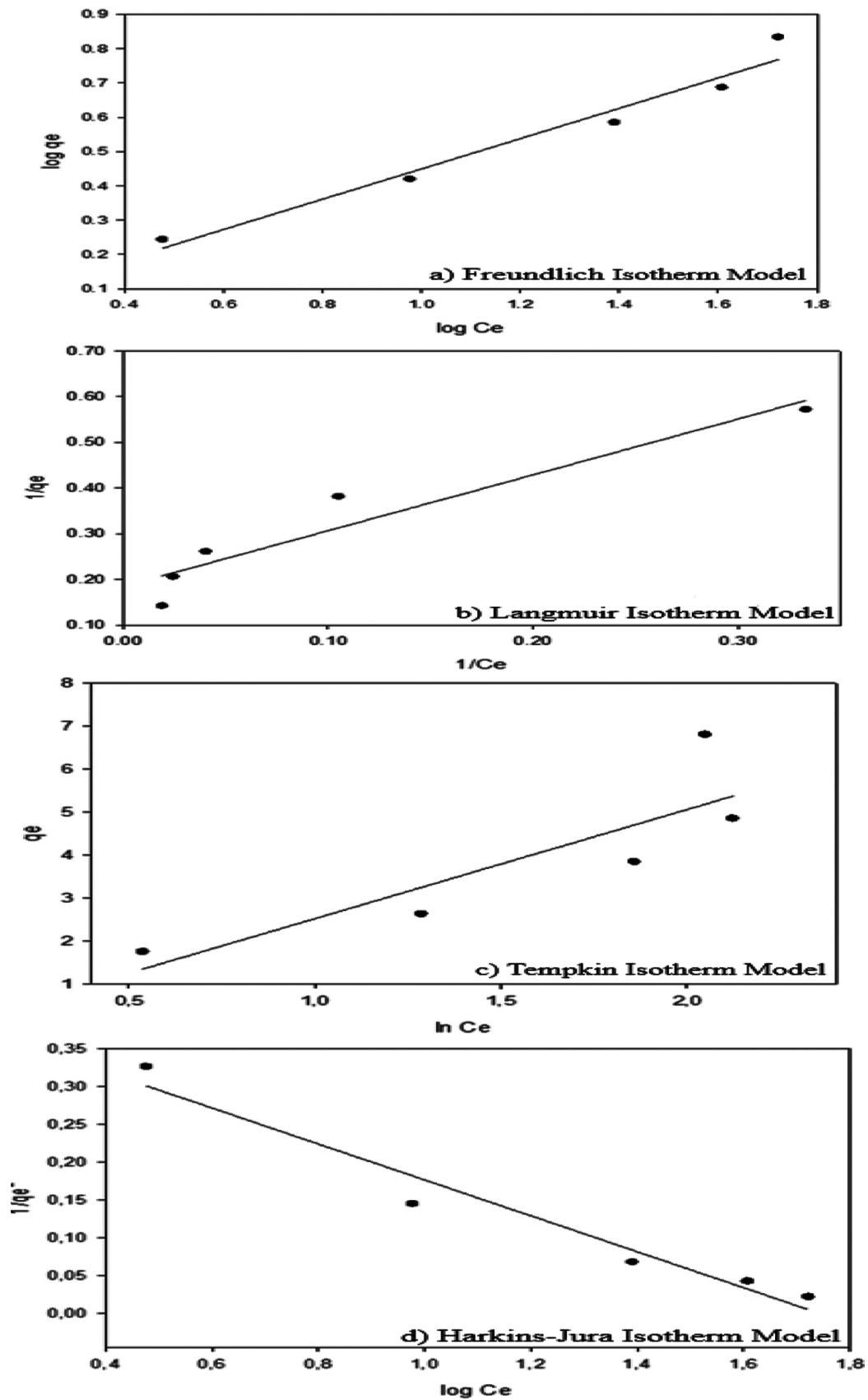


Figure 7. The isotherm modeling results of NPEO adsorption by BT-Fe<sub>3</sub>O<sub>4</sub>.

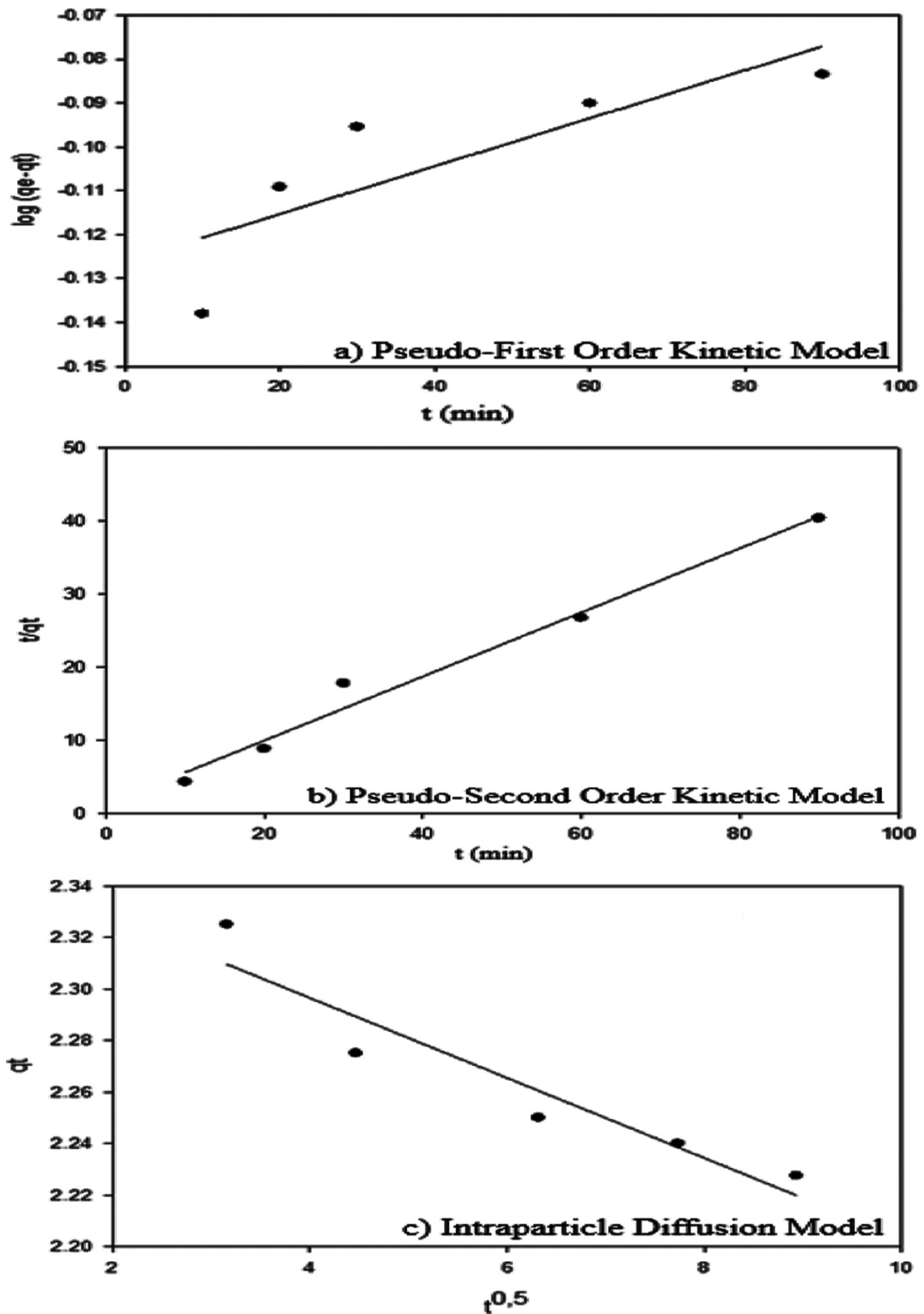


Figure 8. The kinetic modeling results of NPEO adsorption by BT-Fe<sub>3</sub>O<sub>4</sub>.



**Table 3.** The kinetic models and their constants

| Pseudo-First Order Kinetic Model                     |        |        | Pseudo-Second Order Kinetic Model  |        |        | Intraparticle Diffusion Model |        |       |
|--|--------|--------|--|--------|--------|-------------------------------|--------|-------|
| $k_1$  | $q_e$  | $R^2$  | $k_2$  | $q_e$  | $R^2$  | $k_p$                         | $C$    | $R^2$ |
| (l/min)  | (mg/g) |        | (l/min)  | (mg/g) |        | (g.dk <sup>0.5</sup> )        | (mg/g) |       |
| 0.01   | 3.052  | 0.6818 | 18.66  | 2.279  | 0.9817 | 0.015                         | 2.358  | 0.897 |
| $\log(q_e - q_t) = \log q_e - \frac{k_1}{2.303} * t$ |        |        | $\frac{1}{q_t} = \left[ \frac{1}{k_2 * q_e^2} \right] + \frac{1}{q_e} * t$ |        |        | $q_e = k_p t^{0.5} + C$       |        |       |

$k_1$ ,  $k_2$ , and  $k_p$ : constant, C: boundary layer thickness.

**Table 4.** ANOVA analysis

|               |                | SS        | df | MS       | F         | Sig. |
|---------------|----------------|-----------|----|----------|-----------|------|
| pH            | Between Groups | 905.589   | 1  | 905.589  | 1014.188  | .000 |
|               | Within Groups  | 16.073    | 18 | .893     |           |      |
|               | Total          | 921.661   | 19 |          |           |      |
| Nano-dose     | Between Groups | 1035.361  | 1  | 1035.361 | 372729.78 | .000 |
|               | Within Groups  | .050      | 18 | .003     |           |      |
|               | Total          | 1035.411  | 19 |          |           |      |
| Concentration | Between Groups | 1106.789  | 1  | 1106.789 | 1.981     | .176 |
|               | Within Groups  | 10058.491 | 18 | 558.805  |           |      |
|               | Total          | 11165.281 | 19 |          |           |      |

the adsorption process, kinetic experiments were carried out at 25°C with a nano-dose of 1 g/L and 10 mg/L NPEO concentration. The adsorption capacities were determined for the adsorption process of 10-90 min. The kinetic parameters and correlation coefficients ( $R^2$ ) were summarized in Table 3 and Fig. 8 (a, b, and c).

## STATISTICAL ANALYSIS

The empirical results obtained to explain the statistical significance of the proposed adsorption processes were analyzed using ANOVA (Table 4). ANOVA results are directly related to high F-value and low p-value [50]. F-values of the model as 1014.188 and 372729.78 implies the model is significant for pH and BT-Fe<sub>3</sub>O<sub>4</sub> nano-dose, respectively. The probability that such a large F-value will occur due to noise is only 0.01%. P values smaller than 0.0500 showed that the model terms are meaningful. In this instance, pH and BT-Fe<sub>3</sub>O<sub>4</sub> nano-dose are statistically important parameters. Values larger than 0.1000 showed the models are meaningless and the NPEO concentration is a meaningless parameter.

## CONCLUSION

Black tea leaves and Fe<sub>3</sub>O<sub>4</sub> particles were exposed to a green synthesise by chemical co-precipitation method

to obtain BT-Fe<sub>3</sub>O<sub>4</sub> nanoparticles, and these BT-Fe<sub>3</sub>O<sub>4</sub> particles were applied as an efficient adsorbent for the removal of NPEO from a solution. It showed that the kinetic and isotherm models in NPEO removal fit the so-called second-order kinetic and Freundlich models. These models indicated that the process can occur by chemisorption and occur as a multilayer process. The ideal conditions in this paper were defined as pH 7.0, the contact time of 60 min, NPEO concentration of 10 mg/L, and adsorbent dose of 1.0 g/L. Moreover, the extract of black tea leaves was an efficient candidate for the green synthesis of magnetite nanoparticles. The results of this study showed that BT-Fe<sub>3</sub>O<sub>4</sub> particles eco-friendly, cheap-cost particles for the treatment of NPEO from water and wastewater.

## AUTHORSHIP CONTRIBUTIONS

Authors equally contributed to this work.

## DATA AVAILABILITY STATEMENT

The authors confirm that the data that supports the findings of this study are available within the article. Raw data that support the finding of this study are available from the corresponding author, upon reasonable request.

## CONFLICT OF INTEREST

The author declared no potential conflicts of interest with respect to the research, authorship, and/or publication of this article.

## ETHICS

There are no ethical issues with the publication of this manuscript.

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