

DETERMINATION OF SOME DOMESTIC RADIATORS' THERMAL CAPACITY NUMERICALLY

A. S. Dalkilic^{1,*}, O. Acikgoz¹, E. Ekici¹, S. Wongwises²

ABSTRACT

Free convection and radiation comprise the heat transfer mechanisms through which a hydronic household radiator conveys heat from its surface to air and surrounding surfaces. It should also be noted that their performance could be enhanced by improving surface geometries as well as increasing temperature levels. In the present study, heat transfer rates and convective heat transfer coefficients occurring through the investigated radiators, were numerically examined. To this end, radiators at two different dimensions having two different geometric shapes were drawn and analyzed in the program Ansys 17. The heat transfer rates obtained from the program were validated via radiator producer catalogues. Furthermore, the influence of parameters, such as water velocity in the radiators and thus mass flow rate, temperature difference between water inlet and outlet and also between radiator surface and surrounding air on convective heat transfer coefficient over radiator, were scrutinized.

Keywords: Radiator, Heat Transfer, Natural Convection, Radiation, ANSYS

INTRODUCTION

In today's world energy economy agenda, high energy consumption in buildings, has accounted for the requirement for emerging low-temperature heating devices both in new and old ones. Also, energy saving can be achieved by diminishing supply temperatures and radiant panel heating systems that encompass floor heating, ceiling heating and wall heating in central heating systems.

Nonetheless, improving the performance of central heating in buildings has a significant effect on energy savings, as well. Furthermore, heating by radiators has still been the most prevalent technique for domestic and industrial applications in the world. In the usual design of radiators, the hot water is circulated in the narrow radiator channel and heat is conveyed to the ambient air, and the circulated water in the radiator leaves at a lower temperature. Convectors support to rise the heat transfer from the radiators. Computational Fluid Dynamics (CFD) is one of the significant technique to design and improve the performance of the radiator numerically.

Improving the heat capacity of hydronic central heating systems in buildings can be the core point in terms of energy saving. Existing radiators of these systems have working conditions at constant flow plan with thermostat control device mostly. This sort of operating mode may not be evaluated efficient with regard to energy consumption and thus other working scenarios are necessary to improve the heat capacity of the radiators. Given the issues relevant to having better thermal efficiency from radiators, the literature have been thoroughly reviewed and presented in the following paragraphs.

By means of a particle image velocimetry along with a computational fluid dynamics approach, Calisir et al. [1] analyzed the flow of the air over a panel radiator. The inlet and outlet temperatures of the radiator were selected as 75°C and 65°C, respectively. Experiments were carried out on a radiator of which dimensions were 600x1000 mm, under a stable laboratory environment with a room temperature of 20°C. In conclusion, at discrete parts of the radiator, velocity distribution was obtained and figured out that a non-symmetrical velocity distribution took place over the radiator.

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¹Department of Mechanical Engineering, Yıldız Technical University, İstanbul, Turkey

²Department of Mechanical Engineering, King Mongkut's University of Technology and Thonburi, Bangkok, Thailand

*Corresponding Author: dalkilic@yildiz.edu.tr

Orcid id: 0000-0002-5743-3937, 0000-0002-0095-829X, 0000-0002-6000-2863, 0000-0003-2648-6814

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Embaye et al. [2] aimed to study the influence of panel radiator under pulsed flow conditions in order to have indoor spatial temperature and velocity distributions. They stated that they have succeeded energy saving with thermal comfort given by international standards. They benefitted from CFD technique for constant and pulsed flows and validated their results with data in open sources.

Ludumor et al. [3] reviewed automotive engine cooling systems indicating the importance of engine surface temperature regarding with the engine ideal efficiency. They have given latest information on forced engine cooling systems to progress new approaches to increase its efficiency. Parameters affecting the radiator performance from the experimental and numerical works have been summarized briefly.

Calisir et al. [4] aimed to see the influences of the sizes of convectors on heat transfer mainly. Initially, the current convector sizes used in a produced radiator were applied in the code of simulation work. Then, the influences of various sizes about the heat transfer were studied. The primary aim of their work was to investigate an optimum arrangement to have the maximum heat output. The space between two convectors, dimension of the base of the convectors and their tip width was examined, and the maximum heat transfer was achieved for 6.31 mm, 4 mm and 12 mm, correspondingly. It was detected that decreasing the convector height and length has an increasing influence about heat transfer performance. A slight rise in heat transfer was obtained with rising convector thickness, and space between two opposite fins improved the heat transfer to a specified value.

Kayastha [5] used a 55 HP engine radiator data for the numerical analysis. He prepared a model in Pro-E software and solved it in ANSYS-12. Two different pitches around 15 mm and 20 mm are used for helical tubes in the radiator. The comparison is completed for dissimilar mass flow rates in helical type tubes. According to the analyses, maximum temperature drop and minimum pressure drop happen at the mass flow rate of 0.5 kg/sec. It is determined that there is increase in temperature drop and decrease in pressure drop with decreased mass flow rate.

Embaye et al. [6] focused on the effect of pulsed flow parameter on the energy consumption of panel radiators. They modeled two hydronic panel radiators with constant and pulsating flows by CFD technique using the conjugate heat transfer in COMSOL Multiphysics program. The tested radiators were one with single finned surface and one without fins, their sizes were 500 mm long and 300 mm high. They validated their CFD model of the constant flow ones with experimental data in literature successfully. Then, they stated that their simulation results of pulsed flow conditions can decrease the energy consumption of panel radiators in comparison to constant flow ones.

Johansson and Wollerstrand [7] studied on the increase of convection in order to have larger heat output. Their numerical works include the comparison of standard panel radiators with and without add-on-fan blower. They prepared their model by COMSOL software using a 2D-model and the multi physic mode. They tested their model at different temperature levels in the radiator, and at different fan speeds. They aimed to derive new temperature software for the radiator at various fan speeds.

Shi et al. [8] indicated the significance of the optimum design of plate-type radiators. They tried to change the shape of the radiator. They obtained larger efficiencies with the angles of 13-20° for inlet sides of ducts. Their study includes not only numerical simulations, but also it has experimental parts.

Myhren and Holmberg [9] focused on radiator heat output and comfort temperatures in a small office room. They have made tests using different positions for the ventilation air inlet. Their numerical works were performed by CFD software's simulations including visualization of thermal comfort situations. Their conclusions indicated that more stable thermal climate conditions can be obtained by ventilation-radiators under used parameters than the traditional ones. Moreover, they obtained lower radiator surface temperatures by the use of ventilation-radiators and thus energy and environmental savings were able to be obtained.

Sarbu and Sebarchievici [10] studied the thermal performance of various kinds of low temperature heating systems both experimentally and numerically. They compared the heat capacity and comfort of radiator and radiant floor heating systems joined to a ground-coupled heat pump. They prepared a mathematical model with the validation process for the numerical analyses of radiant floors. Furthermore, their comparison work included the energy, environmental and economic performances of floor, wall, ceiling and floor-ceiling heating. They concluded that floor-ceiling heating systems were better than other low-temperature ones relating with having better thermal comfort, lower energy consumption, lower CO₂ emission and lower operating cost.

Aydar and Ekmekci [11] have examined panel radiators in Turkey through CFD codes in three dimensional spaces. They acquired numerical efficiency data and afterward the data were compared with extant catalogue values of panel radiators. Optimum air-side convective heat transfer value was found and as a result of that, computational calculations were carried out in accordance with the determined value.

Chacko et al. [12] issued the airflow distribution in the radiator cover using CFD techniques. A remarkable number of optimization case studies were conducted to determine the optimum configuration of the radiator cover. CFD studies compared with test data have demonstrated that notable fields of re-circulation flows are present in the radiator cover. The optimization provided by means of the CFD work has ensured those recirculation regions to be averted and have augmented the flow within the radiator around 34%.

Sevilgen and Kilic [13] implemented a numerical investigation within a room heated through two radiators, while a virtual manikin having actual dimensions as well as physical shape similar to a real person was sitting. In conclusion, the authors have determined heat interaction between the surfaces of the manikin and the room environment, the local heat transfer coefficients of the manikin and the surroundings etc.

Shati et al. [14] have examined the influence of emissivity and roughness of the surface behind a radiator over the thermal output of the radiator. The numerically and experimentally obtained data have shown that the presence of large scale surface roughness and a high emissivity value enhance not only the heat output, but also the air velocity behind the radiator if it is compared to a smooth surface. The data also demonstrate that the heat transfer may be augmented approximately 26% using a high emissivity saw tooth surface.

Arslanturk and Ozguc [15] developed an analytical model to assess the optimum dimensions of a central heating radiator. They have calculated the optimum geometry that maximizes the heat transfer rate as well as the geometrical limits relevant with manufacturing techniques. Also, the influences of geometrical and thermal parameters over the radiator's efficiency were given.

Menendez-Diaz et al. [16] investigated stoneware panel coverings which are claimed that they enhance the thermal efficiency of radiators. To implement this aim, they carried out a theoretical and experimental work. The results have indicated that within the cooling period, the stoneware panel temperature is a little higher than the corresponding temperature of the aluminum radiator surface of the radiator. Nonetheless, aftermath of the start of cooling, this difference has a tendency to vanish. After 50 minutes cooling has started, the difference was found lower than 2°C.

Brady et al. [17] studied the effect of magnetic decorative covers on the heat output from a radiator. A significant number of case studies were conducted and the heat output a bare radiator was compared with a radiator applied under a magnetic cover, and within a wooden cover. The obtained results have indicated that magnetically applied radiator has a higher efficiency roughly 13-20%, compared to traditional radiator wooden cover.

Kılıç et al. [18] have utilized a CFD approach in order to do the thermal analysis of a steel panel radiator. The study was done according to TS EN442, and the CFD application was executed using finite volume method. It should also be noted that the case studies were implemented under steady-state conditions. As a result, it has been observed that the acquired numerical data are consistent with the relevant experimental data in the literature.

By means of a 3D finite volume CFD code, Jahanbin and Zanchini [19] examined the performance of a thin plane radiator in a real-size room. The case studies they carried out were verified by comparing the mean Nusselt number on the radiator surface with the one attained through the equations derived by some other researchers' in the literature. Using the code, the temperature and velocity fields within the enclosure, the total output of the radiator and the operative temperature have been obtained. As a conclusion, it was understood that a range of 10 cm between radiator and wall provided a small enhancement in air movements within the room.

Beck et al. [20] worked on the effect of wall emissivity behind panel radiators over the heat output. The study was implemented by means of both experimental and numerical methods. The results indicate that the heat transfer can be augmented roughly 20% with the usage of a black wall, instead of a reflective wall. In addition to this, it was stated that the output of single plate radiator would be enhanced approximately 10% and a double radiator roughly 5%.

Furthermore, in his articles Khalifa [21, 22] have scrutinized and presented the convective heat transfer correlations derived by numerous researchers which were found for vertical and horizontal free plates, alongside for enclosures heated through various methods. It should be noted that in the present study, the correlations cited by Khalifa [21, 22] have been selected to compare the results of this study with data in the literature. The correlations chosen, the researchers by whom derived and the conditions they are accurate are presented in Tables 1 and 2.

In case the relevant literature is rigorously scrutinized, it can easily be understood that there has been a significant uninvestigated field regarding household radiators issue. Thus, the influence of numerous parameters that have effects on heat transfer through the radiators, and the convective heat transfer coefficient arising over the radiators have been scrutinized, in the current work. Parameters such as temperature differences at air and water sides, water velocity and mass flow rate were taken in consideration on the calculation of heat output of the tested radiators, and on the convective heat transfer coefficients occurring over them. Moreover, the main purpose of this computational study is to demonstrate the likelihood of validation process of household radiators by means of experimental data, to provide visual clarifications and to produce various outputs using Ansys software's results. The methods of numerically solving this issue and accomplishing this aim consist of examining the internal and external fluid flow of the radiator and then comparing these outputs to the experimental data of a radiator producer company.

NUMERICAL METHOD

Due to long lasting of solution periods, CFD programs were not highly preferable in recent years. Nevertheless, continuously progressing computer processors, in these days allow researchers and building simulators avail themselves of CFD programs in heat transfer applications for heat transfer applications in simulations, such as the radiator systems which consist of different radiator geometries such as in this study. This work, comprised of a broad range of results obtained through varying a number of parameters contains CFD outcomes. To solve the governing equations (continuity, momentum, energy) the CFD program ANSYS 17, which involves FLUENT 17 within, has been preferred. It should also be noted that the outline of the program's solution path is built over the control volume theory through altering relevant equations into algebraic equations for them to be solved. Techniques of control volume are executed by carrying out the integration of the relevant equations on the individual control volume and generating discretization of the equations [23].

One should first be aware of the fact that, to initiate a numerical process, it is significant to separate the given, known data from the unknown one. All sizes for tested radiators are known from producer company's catalogs. The mass flow rates of water regarding the experimental thermal capacities and temperature levels are known. The inlet temperatures for water are taken from catalogs as 75 °C and 90 °C and ambient temperatures varied from 10 °C to 26 °C. The whole numerical process starts with the draw in SolidWorks. Some preferences and automatically determined parameters within the program can be summarized in the following paragraphs:

Among from 5 different size functions, "curvature" has been chosen. Corresponding to Smoothing, Transition, Growth rate options; Medium, Slow and 1.2 selections were made, respectively. Also, minimum edge length of the meshes was 3×10^{-2} . In addition to this, Transition ratio and Maximum layer values have been determined as 0.272 and 5, respectively. As statistical values, it should be noted that 10895 nodes and 46193 elements occurred within the body of the radiator. A gravitational force value at -y direction has been input as 9.81 m/s^2 .

In ANSYS a meshed images of the radiators examined are shown in Figure 1. The next stage is about the entering boundary conditions as water flow velocity, water inlet temperature, ambient temperature and pressure outlet in order to calculate heat transfer rate, surface temperature of the radiator, water outlet temperature, convective heat transfer coefficient of air side, and temperature distribution in the radiator. From this information, it is clear that there are many unknowns for the system. The experimental heat transfer amount is predicted by means of the numerical model in ANSYS 17 of which solution steps are detailed in this section. Some of the obtained numerical results can be seen in Tables 3 and 4 for 900 mm /160 mm and 500 mm/160 mm radiators' 75 °C / 65 °C and 90 °C / 70 °C operating conditions, respectively.

Table 1. The correlations presented Khalifa [21] derived for vertical free plates

Researchers	Conditions	Equation
Churchill and Chu	Range applicable in buildings	$h = \left[0.134(L)^{-\frac{1}{2}} + 1.11(\Delta T)^{\frac{1}{6}} \right]^2$
Alamdari and Hammond	Rayleigh range: 10^4 - 10^{12}	$h = \left\{ \left[1.5 \left(\frac{\Delta T}{L} \right)^{1/4} \right] + \left[1.23(\Delta T)^{\frac{1}{3}} \right]^6 \right\}^{\frac{1}{6}}$
Fishenden and Saunders	Laminar flow	$h = 1.368(\Delta T / L)^{1/4}$
Fishenden and Saunders	Turbulent flow	$h = 1.973(\Delta T)^{1/4}$
Griffiths and Davis	For 1.2 m square plate, up to 100°C temperature difference	$h = 1.776(\Delta T)^{1/4}$
Heilman	Discs up to 0.25 diameter	$h = 1.664(\Delta T)^{0.27}$
King	Correlated data from other researchers	$h = 1.517(\Delta T)^{0.33}$
Hottinger	No note available	$h = 2.5(\Delta T)^{1/4}$
Wilkes and Peterson	Two heated plates 2.4 x 0.8 m ² with 0.1 m air space	$h = 3.05(\Delta T)^{0.12}$
ASHRAE	For laminar flow	$h = 1.42(\Delta T)^{1/4}$
ASHRAE	For laminar flow	$h = 1.31(\Delta T)^{1/3}$
McAdams	For laminar flow	$h = 1.42(\Delta T)^{1/4}$

Table 2. The correlations presented Khalifa [22] derived for enclosures heated through different surfaces

Researchers	Conditions	Equation
Min et al. (heated floor)	Ra range: 10^9 - 10^{11}	$h = 2.416 (\Delta T)^{0.31} / D_e^{0.08}$
Min et al. (vertical wall)	Ra range: 10^9 - 10^{11}	$h = 1.873 (\Delta T)^{0.32} / H^{0.05}$
Min et al. (heated ceiling)	Ra range: 10^9 - 10^{11}	$h = 4.622 (\Delta T)^{0.05} / H^{0.85}$
Li et al.	An occupied office room at working conditions	$h = 2.88(\Delta T)^{0.25}$
Khalifa and Marshall	On vertical wall	$h = 2.30(\Delta T)^{0.23}$

Using the program ANSYS FLUENT 17, a laminar model has been selected owing to entire found Rayleigh number values to be smaller than 10^9 . Also, a steady state solution approach has been seen appropriate. In addition, in order to solve the equations with a high precision, the second order upwind scheme has been chosen to discrete them. The under relaxation factors corresponding to pressure, density, body forces, momentum and energy have been selected 0.3, 1, 1, 0.7 and 0.9, respectively. The necessary time for each case study to converge at the solution was approximately 2 hours.

The residuals for momentum and continuity equations were determined as 10^{-3} , while the value was 10^{-6} for energy equation. Furthermore, thermo-physical properties of the room air have been calculated at the mean surface temperature of surfaces in each case study, through the tables given by Incropera and DeWitt [24]. Moreover, between two solvers presented by FLUENT, pressure based coupled solver along with a SIMPLE scheme have been selected.

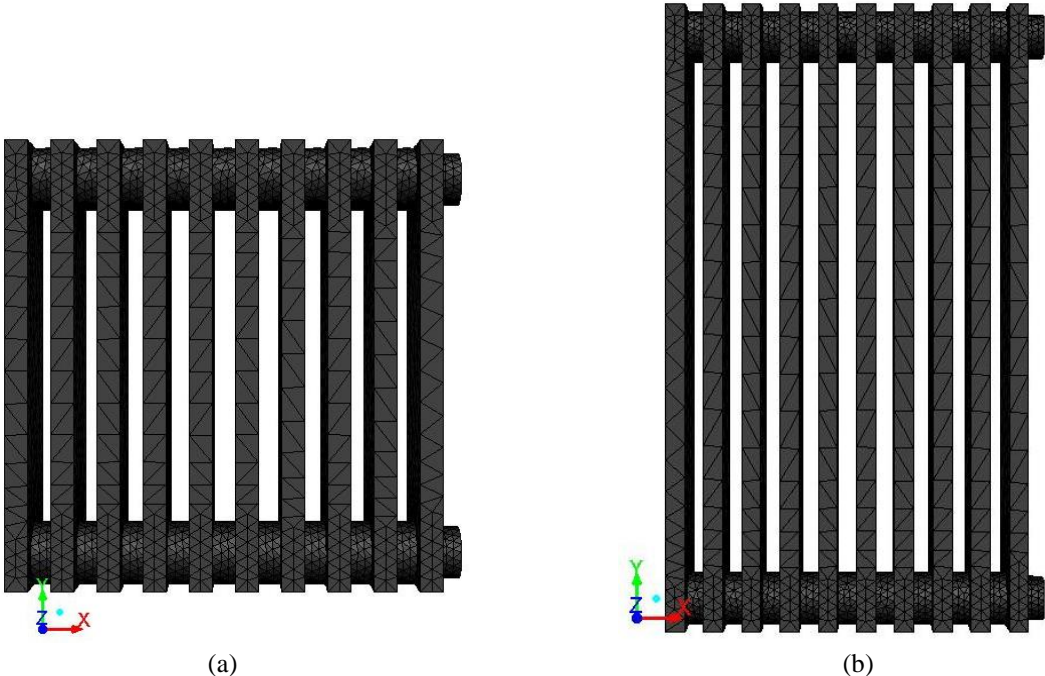
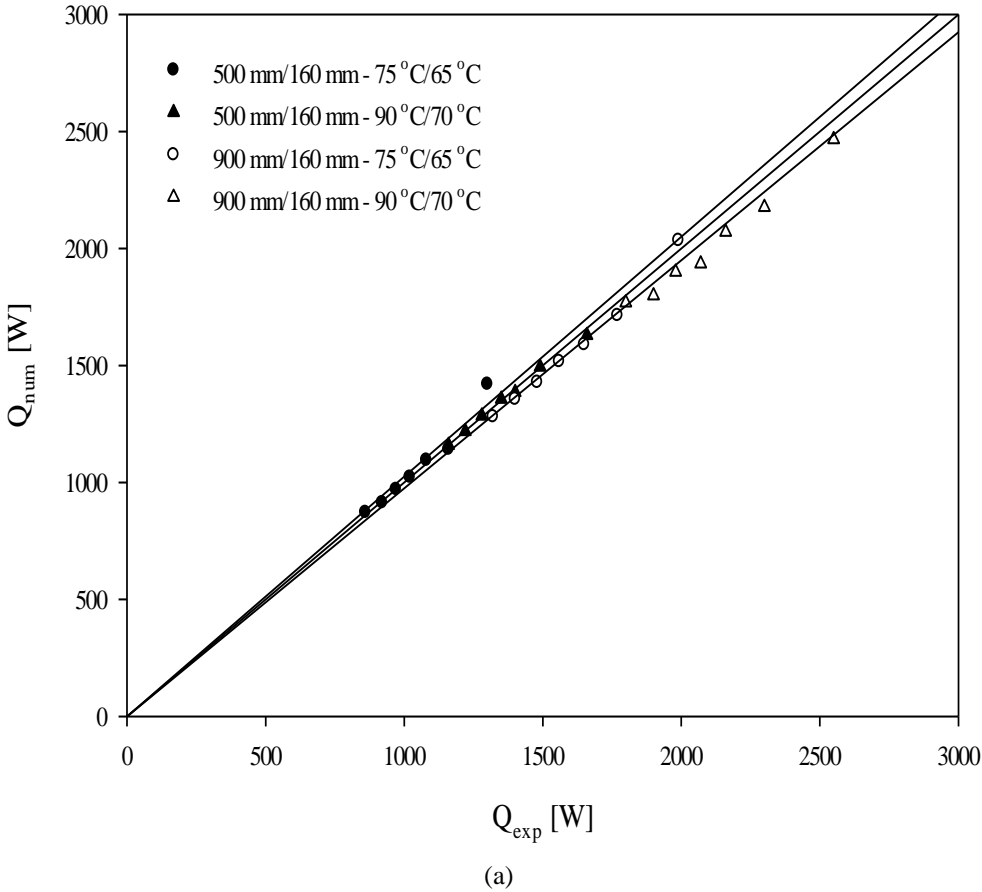


Figure 1. Cornered end radiators used in analyses (a) 500 mm - 160 mm, (b) 900 mm - 160 mm



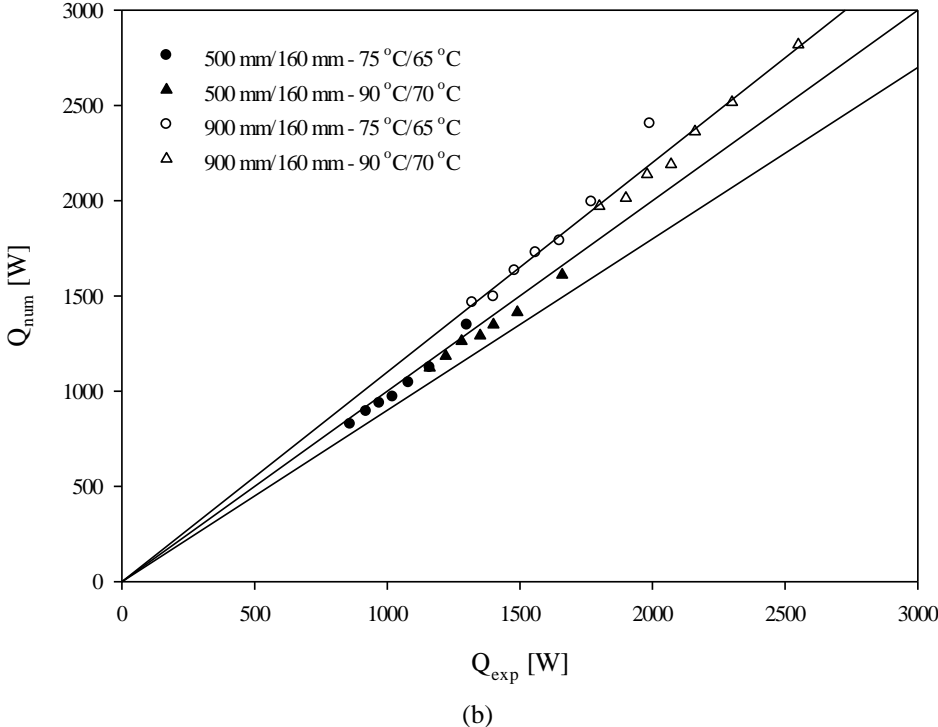
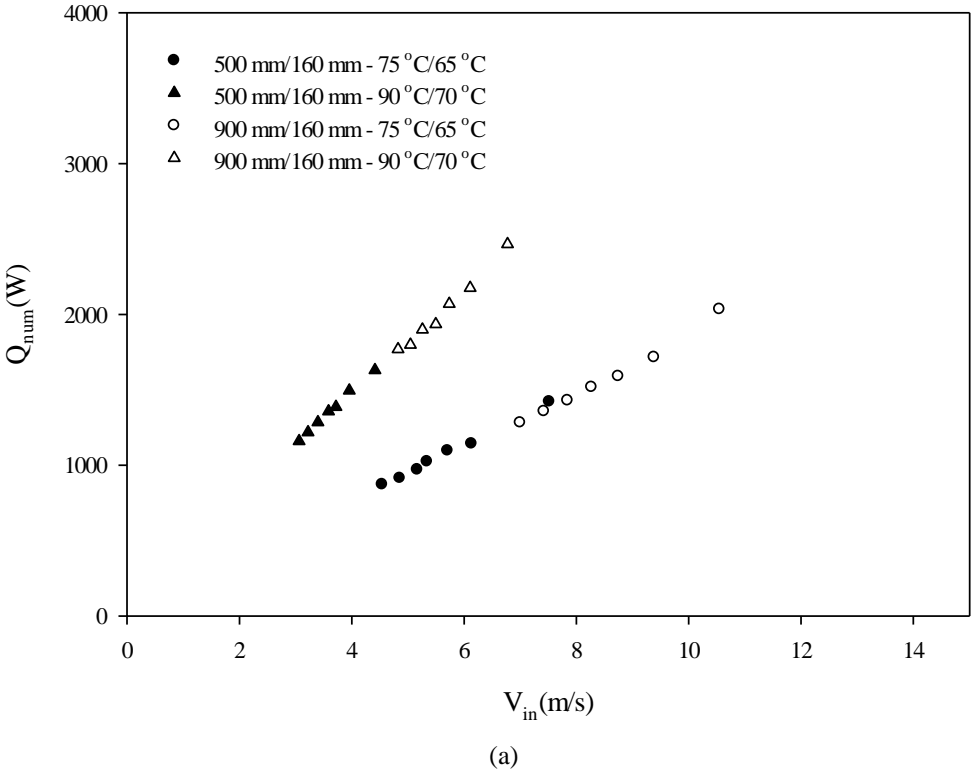
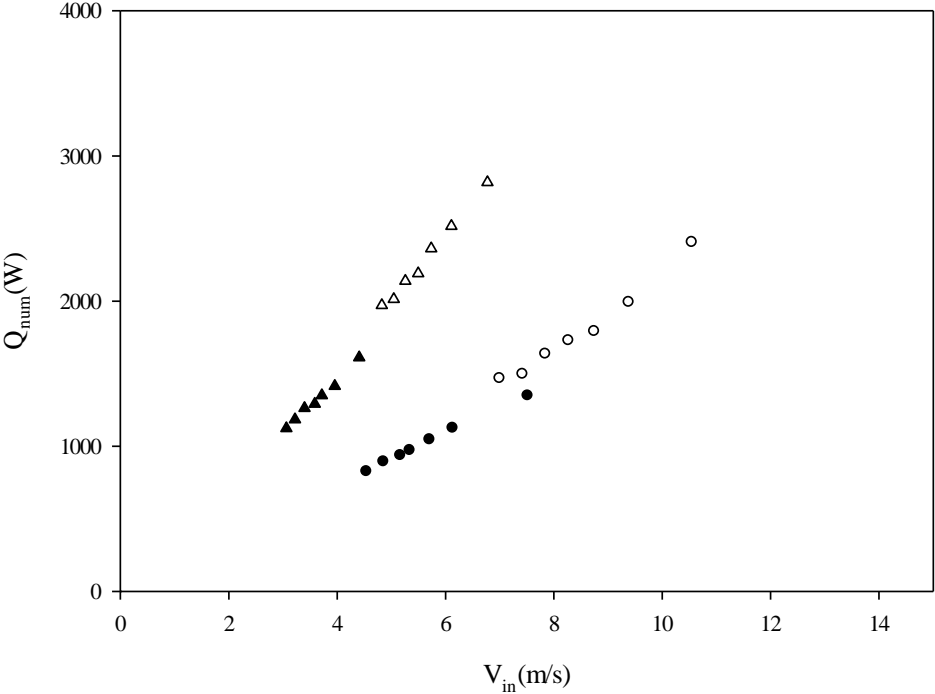


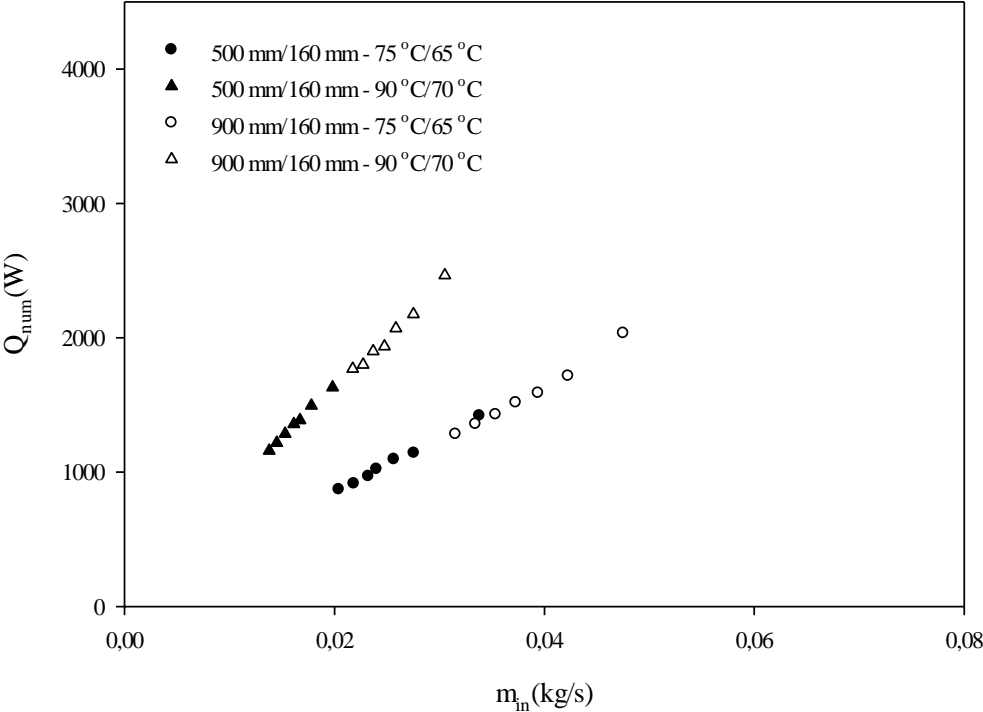
Figure 2. Comparison between the ANSYS total heat transfer values and experimental data (a) for cornered end, (b) for chamfered end radiators





(b)

Figure 3. The variation of total heat transfer rate values with inlet water velocity (a) for cornered end, (b) for chamfered end radiators



(a)

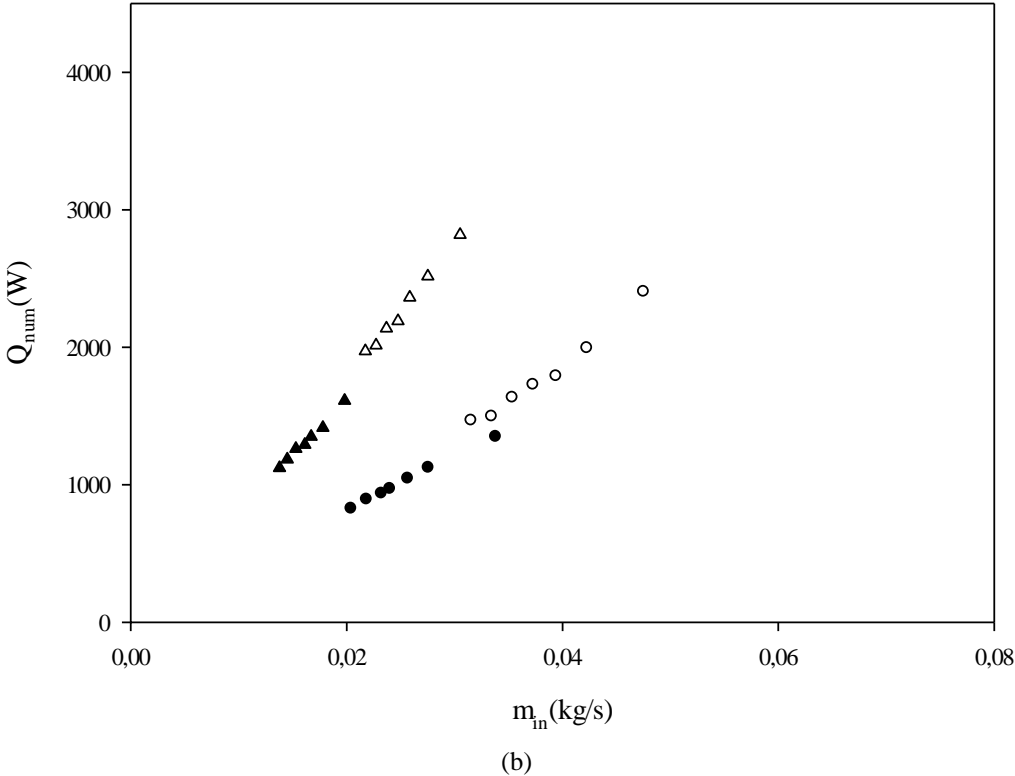
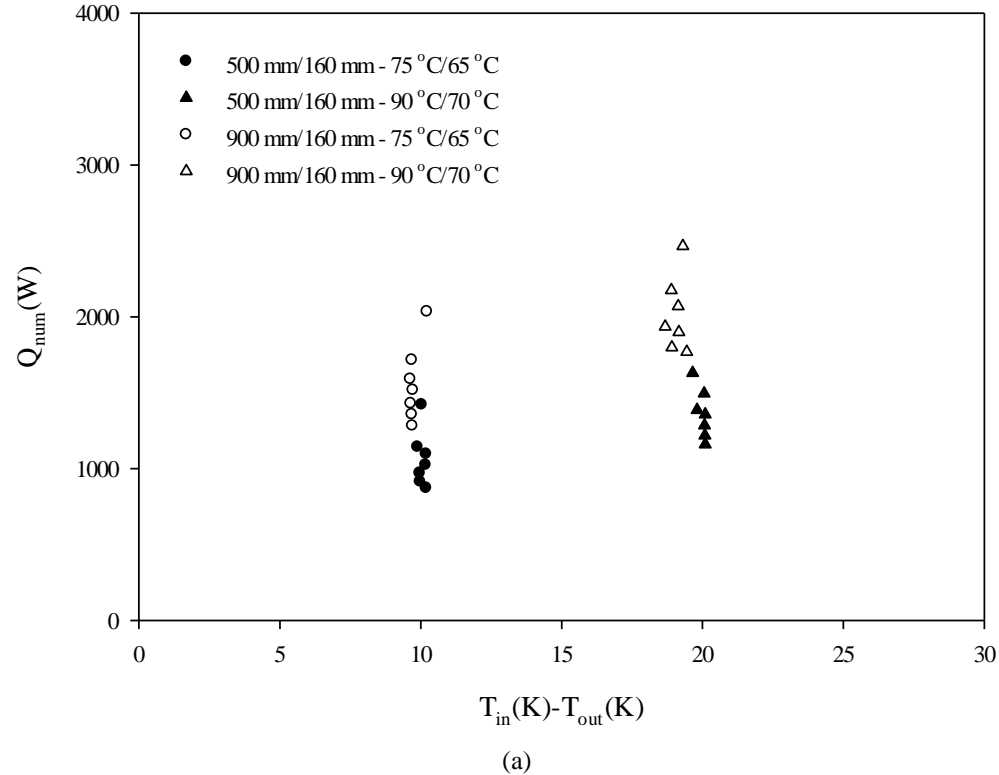


Figure 4. The change of total heat transfer rate found via ANSYS with mass flow inlet (a) for cornered end, (b) for chamfered end radiators



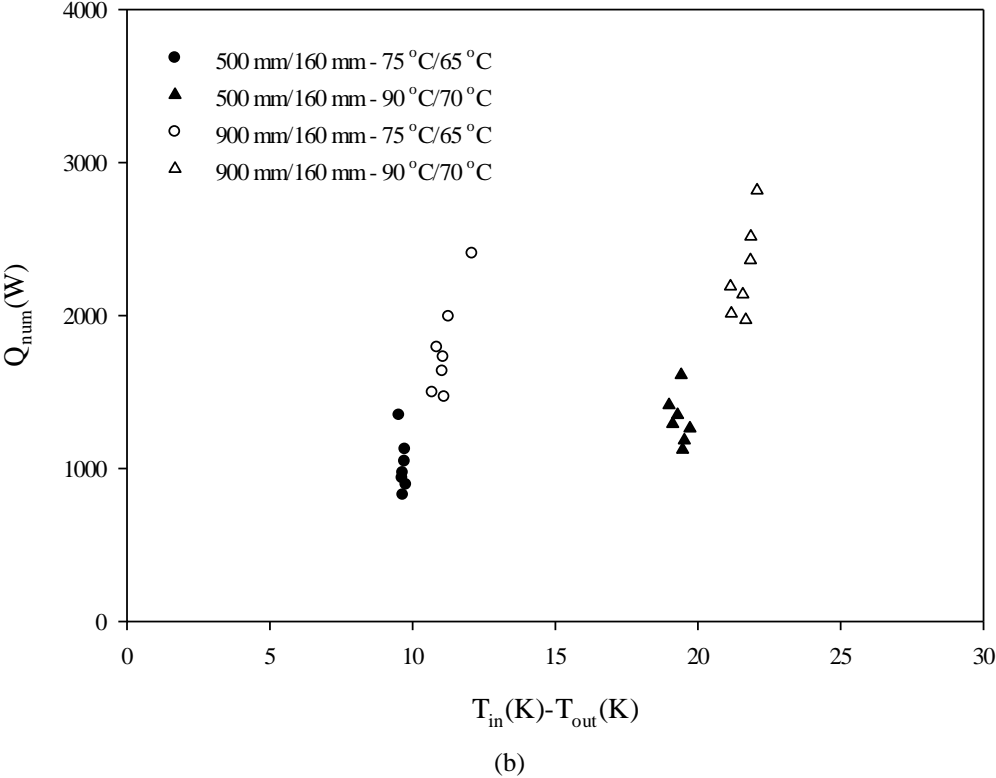
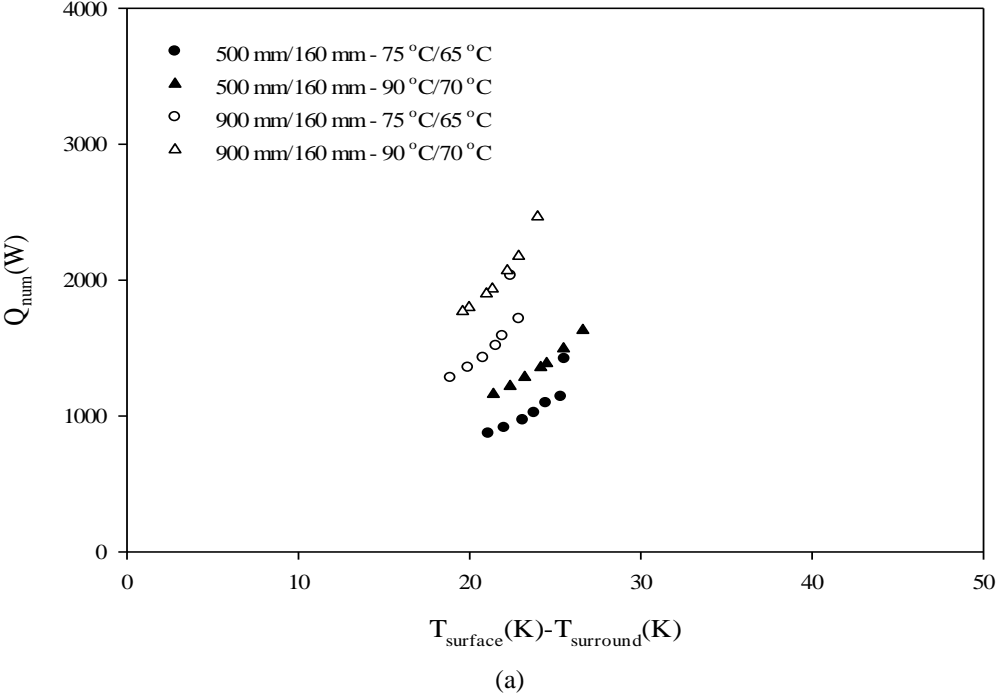


Figure 5. The alteration of total heat transfer rate obtained via ANSYS with radiator inlet and outlet temperature difference (a) for cornered end, (b) for chamfered end radiators



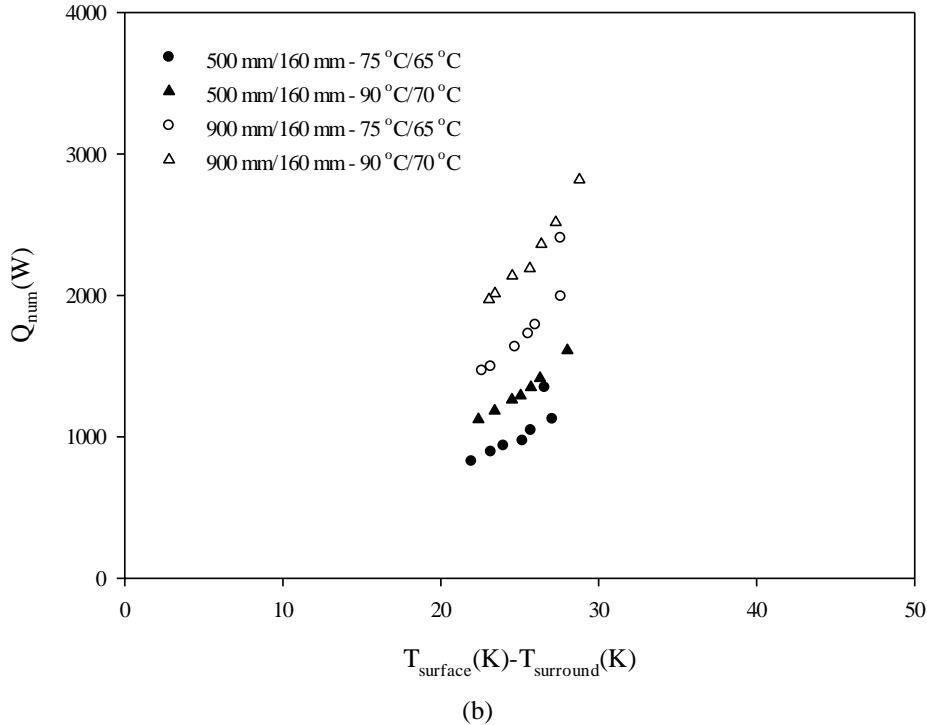
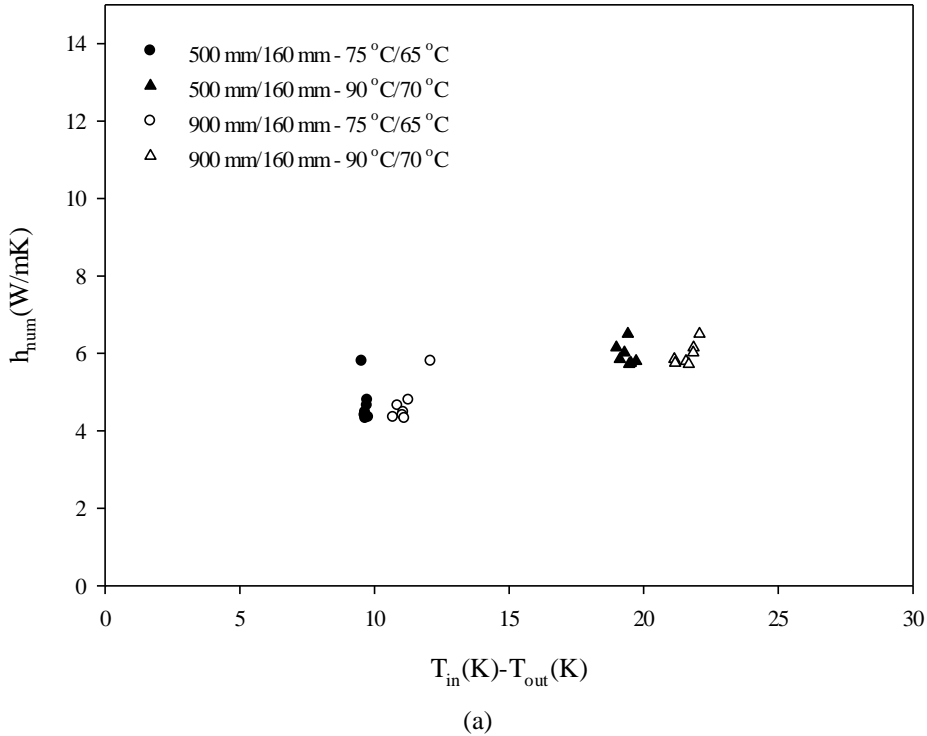


Figure 6. The variation of total heat transfer rate obtained via ANSYS as the temperature difference between radiator surface and air varies, (a) for cornered end, (b) for chamfered end radiators



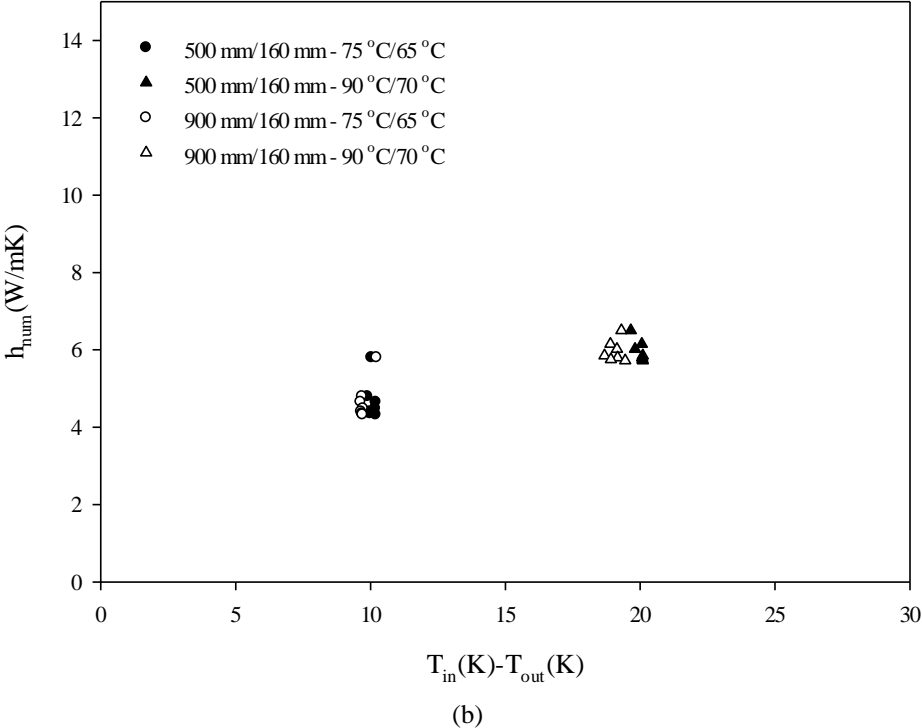
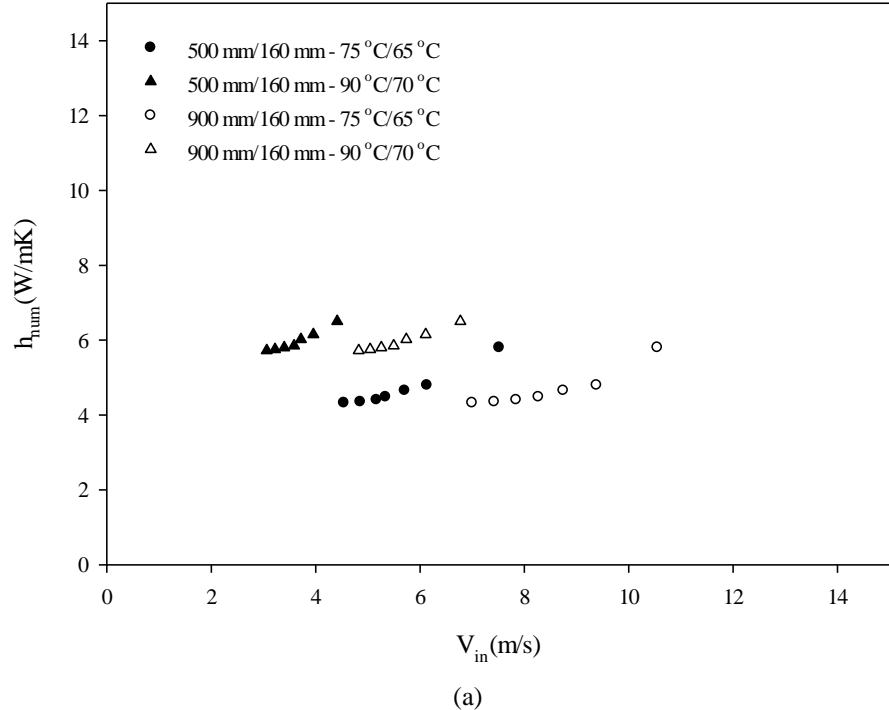


Figure 7. The change of convective heat transfer coefficient occurring over the radiator, with the variation of the temperature difference between radiator inlet and outlet temperatures, (a) for cornered end, (b) for chamfered end radiators



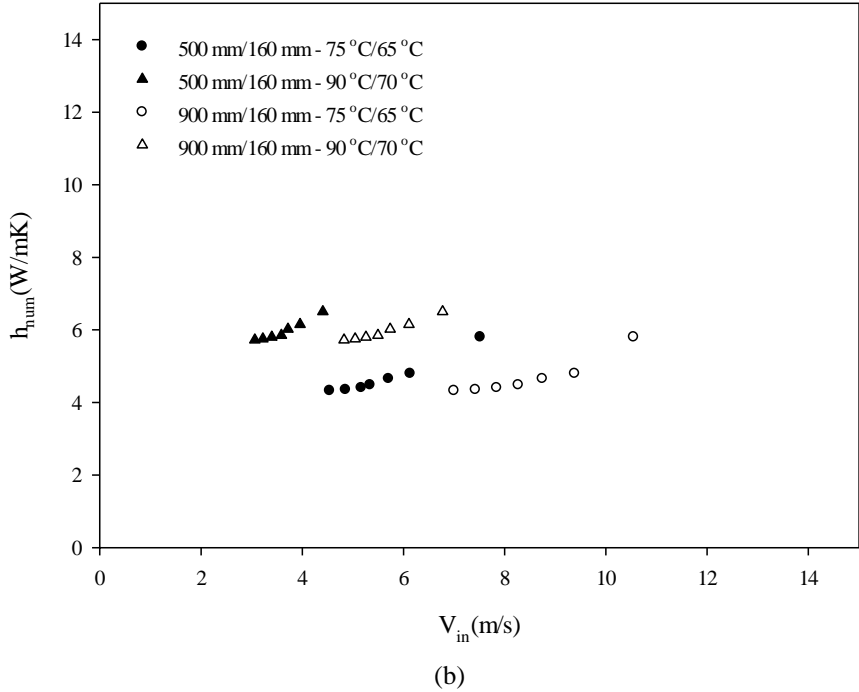
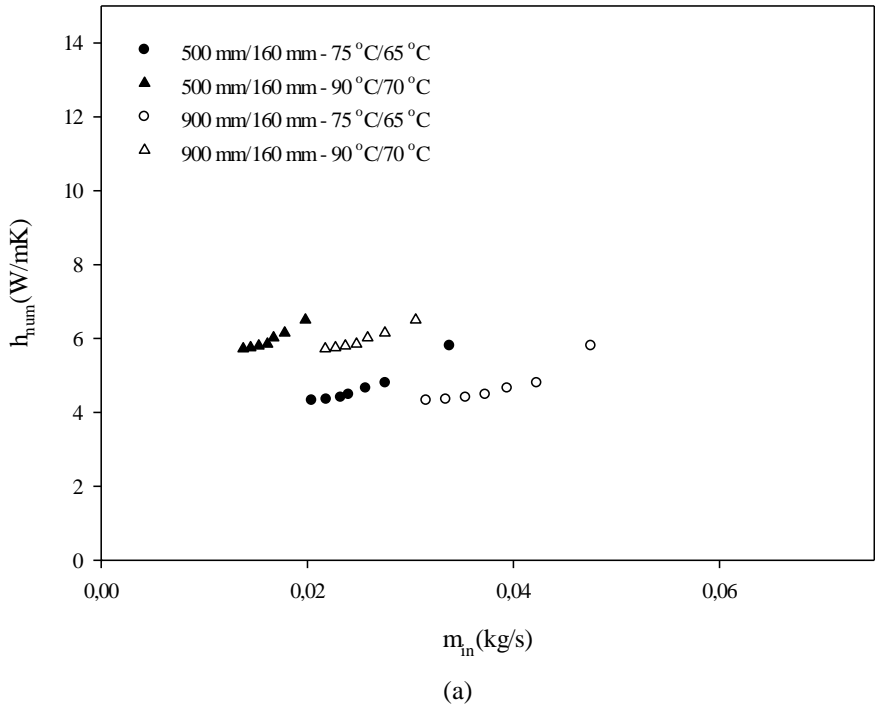


Figure 8. The variation of convective heat transfer coefficient values with inlet water velocity (a) for cornered end, (b) for chamfered end radiators



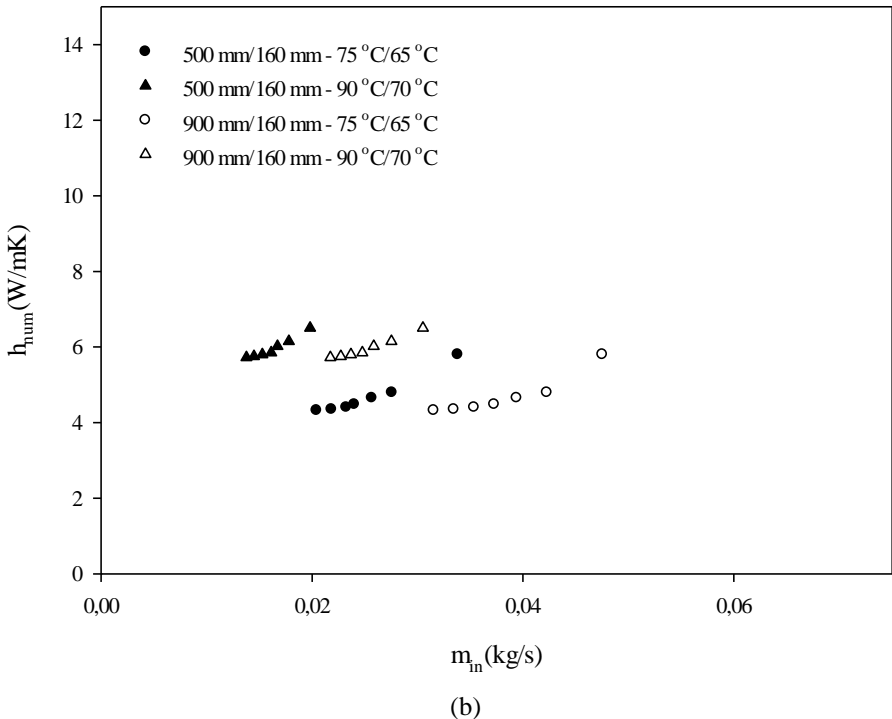
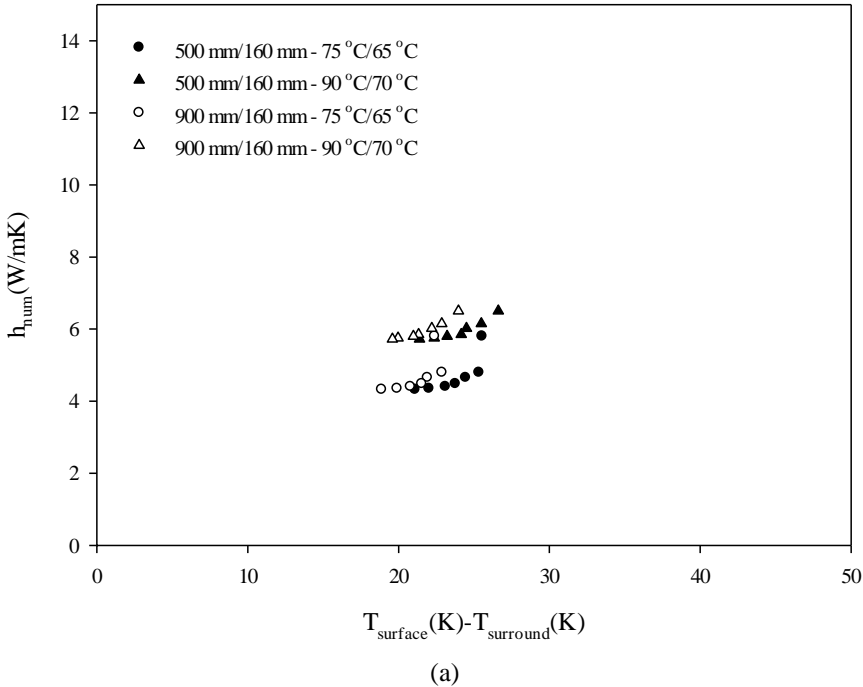


Figure 9. The change of convective heat transfer coefficient with mass flow inlet (a) for cornered end, (b) for chamfered end radiators



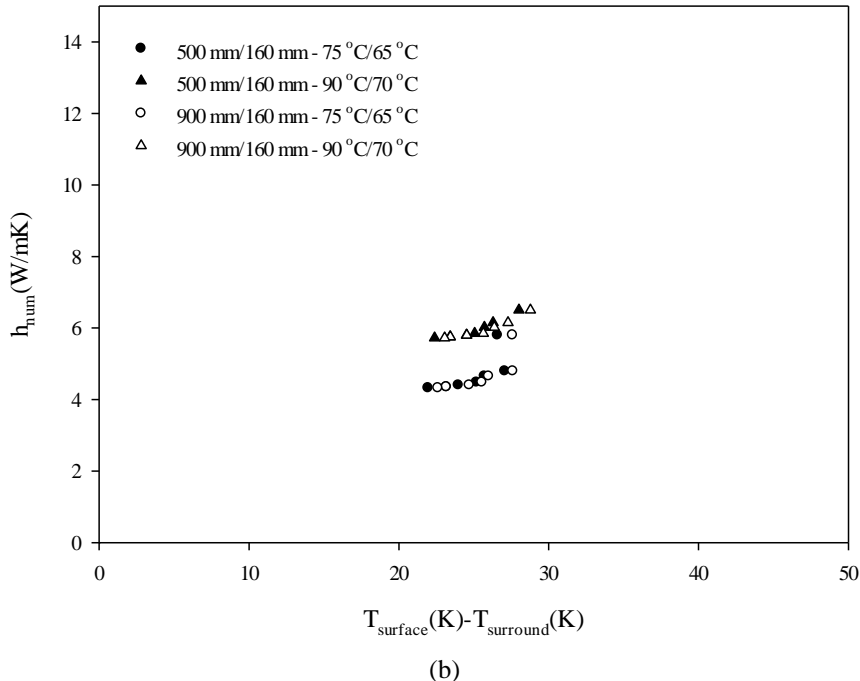
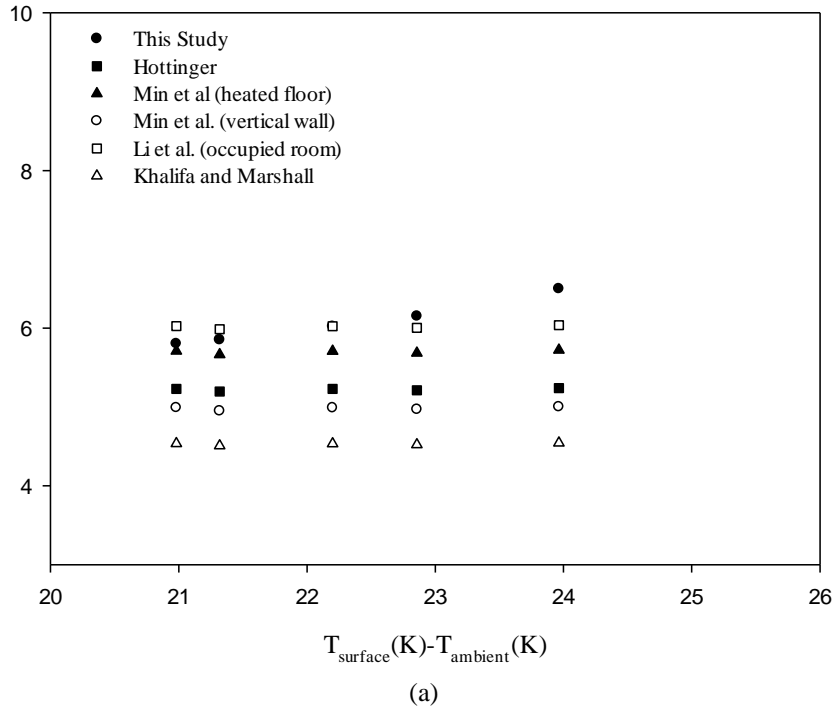


Figure 10. The variation of convective heat transfer coefficient obtained via ANSYS as the temperature difference between radiator surface and air changes, (a) for cornered end, (b) for chamfered end radiators



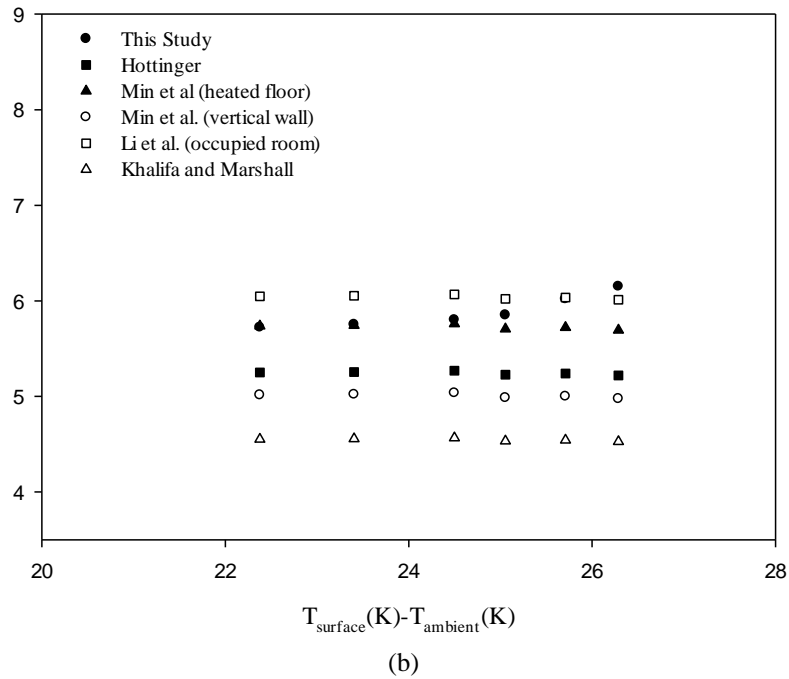


Figure 11. Comparison between the results of this study and the results obtained using the correlations derived by other researchers, (a) for a cornered end 900 mm/160 mm 90°C/70°C radiator, (b) for a chamfered end 500 mm/160 mm 90°C/70°C

Table 3. Some of the operating conditions and findings of 900 mm -160 mm radiator for 90 °C / 70 °C

(900 mm - 160 mm) (90 °C / 70 °C) Cornered End Radiator								
W/m ² K	m/s	K	K	Watt	Watt	%	K	K
h	v _{in}	T _{in}	T _{out}	Q _{num}	Q _{exp}	Error rate	T _{surface}	T _{ambient}
6,5	6,77	363	343,69	2465,76	2550	3,30	306.96	283
6,15	6,10	363	344,10	2176,20	2300	5,38	310.86	288
6,02	5,73	363	343,86	2070,41	2160	4,14	313.20	291
5,85	5,49	363	344,32	1935,40	2070	6,50	314.32	293
5,8	5,25	363	343,83	1899,97	1980	4,04	315.98	295
5,75	5,04	363	344,08	1799,20	1900	5,30	316.96	297
5,72	4,82	363	343,55	1768,67	1800	1,74	318.59	299

Table 4. Some of the operating conditions and findings of 500 mm -160 mm radiator for 90 °C / 70 °C

(500 mm - 160 mm) (90 °C / 70 °C) Cornered End Radiator								
W/m ² K	m/s	K	K	Watt	Watt	%	K	K
h	v _{in}	T _{in}	T _{out}	Q _{num}	Q _{exp}	Error rate	T _{surface}	T _{ambient}
6.5	4.41	363	343.35	1629.942	1660	1.81	309.617	283
6.15	3.95	363	342.937	1494.397	1490	-0.29	313.485	288
6.02	3.71	363	343.191	1385.869	1400	1	315.492	291
5.85	3.58	363	342.901	1356.829	1350	-0.5	317.144	293
5.8	3.39	363	342.929	1284.305	1280	-0.33	318.215	295
5.75	3.22	363	342.918	1218.02	1220	0.16	319.357	297
5.72	3.06	363	342.902	1159.013	1160	0.08	320.38	299

RESULTS AND DISCUSSION

The main purposes of this study are to numerically find heat transfer characteristics occurring over the household iron casting radiators produced by a company, and to compare the obtained numerical results with experimental results of the producer in terms of heat transfer rates, and also compare the numerically calculated convective heat transfer coefficient values with the results found by executing the correlations derived by researchers cited in Tables 1 and 2.

Figures 2a and 2b illustrate the comparison between the experimental data and the numerically obtained values with this study. At different radiator dimensions, as well as, inlet and outlet temperatures, it is observed that numerically acquired data predicts the experimental results of the radiator company within 5% and 10% deviation ratios for cornered end and chamfered end radiators, respectively. This comparison proves the correctness of the computational model performed in the present study.

Figures 3a and 3b demonstrate the increase in heat transfer rate through the radiators at different radiator sizes and water inlet and outlet temperatures, and at cornered end and chamfered end radiators, respectively. As expected, the more water velocities in radiators result in the rise in forced convection and thus heat transfer rate ascends. It is also obvious that the increase on radiator dimensions has led to a sharp increase in heat transfer rate. Very similarly, as shown in Figures 4a and 4b the increase in mass flow rate flowing in radiators at different dimensions and inlet/outlet temperatures accounts for the augmentation on radiator's heat transfer rate.

Figures 5a and 5b reveal that at the same radiator inlet and outlet water temperatures, as the radiator dimension rises from 500 mm to 900 mm, the heat transfer rate of the radiator shows a notable increase, for cornered end and chamfered end radiators, respectively. Moreover, it is evident that at the same radiator dimensions, with ascending values of water inlet temperatures, the heat transfer rate values illustrate a remarkable advance. Additionally, the data illustrated in Figures 6a and 6b demonstrate the augmentation in heat transfer rate of radiators with increasing values of temperature difference between surface and surrounding air temperature, at cornered end and chamfered end radiators, respectively.

Figures 7a and 7b shows the convective heat transfer characteristics occurring over the radiators and their variation with inlet and outlet temperature difference values. It can be observed that at different radiator dimensions (500 mm and 900 mm) and at the same radiator inlet and outlet temperatures, the convective heat transfer coefficient draws very slight variations, whereas, it shows a more remarkable change as the abovementioned temperature difference rises, when dimensions are the same.

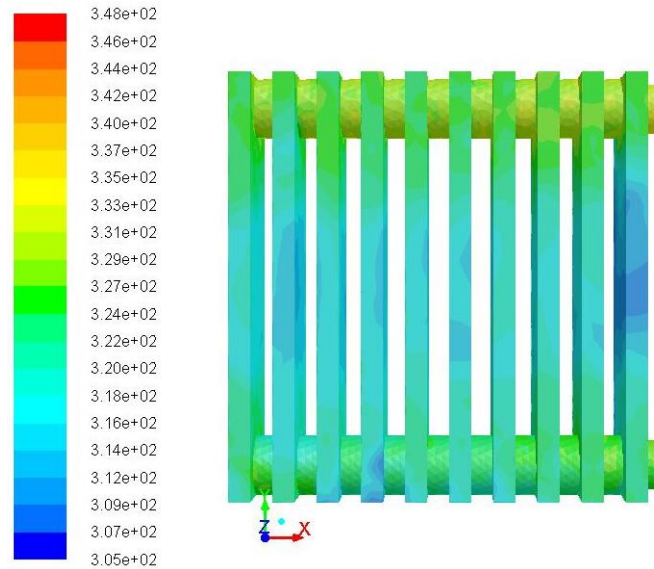


Figure 12. Temperature distribution on the surface of 500 mm – 160 mm radiator in 26 °C ambient temperature

Figures 8a and 8b illustrate the alteration of convective heat transfer coefficients over radiator surfaces with water velocity inlet values to the radiator. Similar to the Figures 3a and 3b demonstrating the change of heat transfer rate with velocity inlet values, the convective heat transfer coefficient values also rise with increasing velocity inlet values, since higher values of velocity have induced forced convection at higher levels within the radiator and therefore causing higher values of convective heat transfer coefficients over the radiator. In a very similar trend, Figures 9a and 9b draw the variation of the convective heat transfer coefficient with changing values of mass flow rates in radiators, for cornered end and chamfered end radiators, respectively. It is clear that with an increase in mass flow rate, in all case studies, the convective heat transfer coefficient demonstrates a noticeable growth over the radiator surface.

In Figures 10a and 10b show the change in convective heat transfer coefficient with the temperature difference between surface and surrounding air temperatures. From the figures, it can be seen that as the aforementioned temperature difference grows, due to increasing air movements over the radiator, the convective heat transfer coefficient ascends. Also, as expected, this coefficient illustrates a clear increase as the radiator water inlet temperature rises from 90°C to 75°C. Moreover, it should be noted that a very slight increase on this coefficient could be observed while one dimension of the radiators descends from 900 mm to 500 mm.

In addition to the validations implemented with experimental data in Figures 2a and 2b, the results obtained through the present work were compared with the data found utilizing correlations explored by some other researchers in the literature. In Figures 11a and 11b, for a 900 mm/160 mm cornered end, and for a chamfered end 500 mm/160 mm radiator, respectively, this comparison has been made. It is evident through the figures that the results of the present study lie within the range of the data acquired by executing the correlations cited in these figures. It should be noted that the sole successful correlation predicting the results of the current study which has been derived for free plates, is Hottinger's correlation, with an average deviation ratio of 4.08%. On the other hand, the correlations explored for enclosures have enabled much more consistent outputs with the results of this study. While the correlations proposed for heated floor and vertical walls by Min et al. deviate by 0.72% and 12.55% at average, respectively; the correlation of Li et al. obtained for an occupied office room under normal working conditions, deviates at an average value of 10.5%.

Figure 12 illustrates an image via Ansys, displaying the temperature distribution in one of the tested radiators which was abovementioned and presented in Figure 1. The influence of heat loss from hot water to surrounding air is noticed through this figure obviously.

CONCLUSION

As well as the thermal capacities of household radiators, convective heat transfer coefficient values occurring over their surfaces comprise the most crucial issues in terms of energy economy and thermal comfort. From this point of view, in the present study, a numerical model investigating household radiators at different dimensions, water inlet temperatures, inlet velocities and geometric shapes was generated by means of the program Ansys 17.

To obtain a The radiators were simulated using wide range of input ambient temperature conditions from 10 °C to 26 °C and water velocity ranging from 3.06 m/s to 7.51 m/s for 500 mm/160 mm type radiator and 4.82 m/s to 10.54 m/s for 900 mm/160 mm type radiator. The deductions obtained were summed up as follows:

The heat transfer capacity and the convective heat transfer coefficient over the radiator increase with increasing values of water inlet velocity and also mass flow rate, due to growing values of forced convection within radiators.

Using a producer's catalogue, found thermal capacity values and also the model developed at different dimensions, geometric shapes and water inlet temperatures, have been validated within the deviation values of 5%, and 10%, for cornered end, and chamfered end radiator types, respectively.

The results regarding the convective heat transfer coefficient values were compared with the data obtained using the correlations found by some other researchers, and noticed that a favorable consistency has been achieved.

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NOMENCLATURE

h_{num}	convective heat transfer coefficient, W/m ² K
m_{in}	mass flow rate, kg/s
Q_{exp}	experimentally found thermal capacity, W
Q_{num}	thermal capacity, W
T_{in}	inlet temperature, K
T_{out}	outlet temperature, K
$T_{surface}$	radiator surface temperature, K
$T_{surround}$	surrounding air temperature, K
v_{in}	velocity inlet, m/s
exp	experimental
in	inlet
num	numerical
out	outlet

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